

LEACHATE RETENTION AT VOLCANIC WASTE LANDFILLS
USING HORIZONTAL INJECTION

By

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LUDICRATE CYCLOCYCLE AT POLYMER WASTE LANDFILL
DURING INJECTION INJECTION

by

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Major Department: Civil and Environmental Engineering

A method of leachate recycle known as horizontal injection was examined. In this method, leachate is introduced to a landfill through horizontal trenches or wells buried within the landfill. Potential advantages of a leachate recycle system of this nature include the ability to recycle leachate to the landfill without atmospheric exposure, the ability to control the point of leachate recycle and the resulting solute distribution, and the ability to limit impact of leachate recycle on daily landfill operations.

Analytical equations were developed to describe the expected shape of the saturated zone surrounding an injection line for both isotropic and anisotropic conditions. The equations were developed by treating an injection line as a

the source in a porous medium subject to a gravity drainage flow field. Capillary forces and dispersion were neglected. The equations allowed prediction of the horizontal and vertical spread of the saturated zone and the resulting injection pressure as a function of injection line length, flow, and waste hydraulic conductivity.

A horizontal injection trench recycle system configuration was constructed and operated at a Florida landfill. The system consisted of perforated pipes placed in screened trench filter sections and buried between lifts of compacted solid waste. The performance of 11 injection lines was evaluated during a period of 15 months. 1.4 million gallons of benzene were recycled to the landfill through the injection system. Pressures and flows observed during the injection were recorded. Typical injection line responses ranged from 0.005 to 0.007 gpm/ft per foot greater extension of applied pressure head in trenches with shored walls as a drainage blanket. In trenches without walls, flow rates ranged from 0.004 to 0.008 gpm/ft per foot of applied pressure head. Injection at high pressures did result in some surface seepage from injection lines located near the margin of the landfill.

CHAPTER 1 INTRODUCTION

Landfill waste recycling, also referred to as landfill regeneration, is a process of recovering materials at solid waste landfills. This process involves the return of recovered materials by a landfill liner and landfill collection system back to the landfill with waste. Recovery sites for landfill recycle include leachate volume management, leachate treatment, concentrated landfill stabilization, and enhanced gas production. Previous pilot-studies have been performed demonstrating these benefits (Feldman 1978, Gray, Laskin et al. 1979, Misch et al. 1983).

Landfill recycle has been positioned at full-scale landfills in the United States and Europe (Berger and Berndt 1994, Jacobs and Robertson 1998, Helman 1997) but the results of these projects as regard to the performance and design of various methods of landfill recycle have been limited. The most recent guidance to regulators of the Resource Conservation and Recovery Act permit landfill recycle in properly designed landfills (Federal Register 1993), but the potential is discouraged by some state regulators as a result of potential threats from poorly operated systems. Further investigation into the similarities involved in various methods

of leachate recycle is necessary to allow safe and effective design of leachate recycle systems at landfills, and for the development of regulations and the transfer of this technology.

This dissertation discusses a leachate recycle process known as horizontal injection and reports its application at an operating landfill in Alachua County, Florida. In this process, leachate is pumped under pressure into horizontal injection lines buried at various depths within the landfill. This method of leachate recycle has a number of potential advantages over other methods including limitation of leachate exposure to the atmosphere, ability to control points of leachate application and leachate circulation, and minimized interference of leachate recycle operations on overall landfill operation.

In Chapter 2 of this dissertation, mathematical equations are developed to describe the shape of the plume emanating from injection lines under steady injection conditions as a function of injected flow rate and the hydrodynamic conductivity of the medium. Isotropic and anisotropic conditions are considered. Chapter 3 presents information on the design, construction, and operation of the horizontal injection-leachate recycle system (HILS) at the Alachua County landfill, and discusses the results and performance of the system. Chapter 4 uses the information in Chapters 2 and 3 to utilize simulation and operation

guidelines, and a design procedure for use of torquated injections as a method of isolating people in operating buildings. A summary of the dissertation and conclusions reached from the research, as well as areas of additional needed research, are presented in Chapter 8.

CHAPTER 2
SATURATED FLOW FROM A HORIZONTAL INJECTION
LEACHATE RECYCLE SYSTEM

INTRODUCTION

Horizontal injection leachate recycle involves the infiltration of leachate to a landfill through the use of horizontal recharge wells. The wells are buried within the waste, and are usually constructed on the waste or deposited. Horizontal injection leachate recycle systems (HILS) represent a promising technology for leachate and solid waste management at landfills, but such systems are relatively untested and little information is available on their design. This chapter outlines analytical equations which describe the characteristics of steady state saturated flow of water surrounding a horizontal well resulting from the pressure of the injected water and gravity. This chapter was developed as proposed by, but independent of, a R1-LHS under evaluation as a tool useful in Florida (Chapter 3).

The method outlined here to model the saturated zone of water which surrounds a horizontal injection well is based on the assumption that the well can be treated as a punctuated line source. The line source is subject to the effect of gravity in the vertical downward direction. It further assumes by rule that water movement is not impeded in the

downward direction. This case occurs in (1)and (2)(b) where a highly conductive vadose layer extends transverse to the linear aquifer.

Simulations of water flow from linear sources buried in soil/air has been performed in the well-known field in a number of previous investigations (Carte 1970, Philip 1971, Beckman and Thomas 1973, Thomas et al. 1980). The primary driving force for water movement in these irrigation studies has been the capillary action of the soil. These analyses have simulated the unsaturated moisture profile resulting from capillary forces, and describe conditions at relatively low flow. The resulting solutions are generally complex, multi-layered equations.

The process utilized here to describe the saturated zone surrounding a horizontal injection well involves the assumption that the primary driving forces for solute transport are the presence of the injected water and gravity. If capillary forces and the effects of dispersion are neglected, a single analytical solution describing the shape of the saturated zone may be determined. The resulting solution is similar to the relation of groundwater recharge through a vertical well in a confined aquifer subject to a uniform field of flow (van and Jacobs 1954). The solution of the uniform flow field analysis has also been applied to the development of capture zone equations in the management of pollutant plumes in groundwater (Vanderford and Cole-Pal 1984).

The solution flow field in the vertical well annulus is analogous to the gravity drainage flow field in this analysis. An advantage to the treatment of the flow system in this manner is that a solution for the case of an immobile material is readily obtained.

Injection flow and capillary forces certainly play a role in solute transport under typical landfill conditions. In the annulus model, a capillary fringe at water level divides surrounding the saturated zone. The equations utilized here are not intended to provide a method of calculating complex water balance and solute trapping conditions for landfills with capillary models which incorporate saturated and unsaturated flow and which account for the complication of multiple well systems are necessary. It is proposed in this chapter, however, that for purposes of establishing design boundaries for efficient and safe design operation at maximum flow conditions, saturated flow hypotheses can be used to estimate requirements for injection well spacing, depth, pressure requirements, and leachate collection system design.

Model Development

A schematic of the flow system analyzed is presented in Figure 2-1. The horizontal injection well is located with its center at the origin and is represented by a line segment. The well consists of two finite radius (r_w) tube in injection into the well at a flow rate of q , which represents the linear

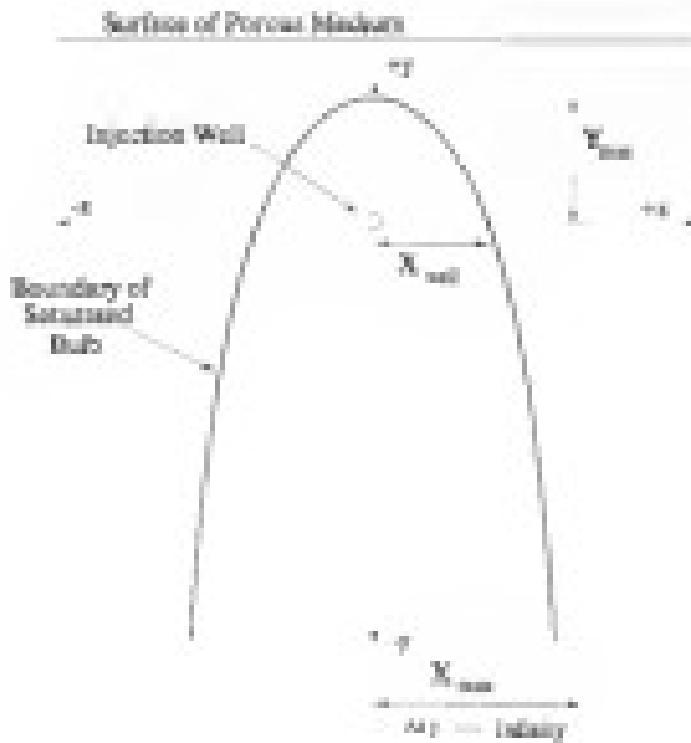


Figure 3-3 Illustration of Flow Fields Surrounding a Horizontal Injection Well Flow System under Steady Conditions.

flow rate (flow per unit length of well), under steady conditions, a saturated zone will form around the injection well, reaching some maximum height above the well, Y_{sat} . If V_{sat} is the potential of a fluid particle to move away from the well in equal to the potential created by gravity to move toward the well, and a parabolic point envelope, it is assumed that the flow domain beneath the well without resistance, the width of the saturated front at an intrinsic downward distance is R_{sat} . The distance from the origin to the edge of the saturated front at the elevation of the well is defined as R_{sat} .

Flow in isotropic media

The analysis of saturated flow from a horizontal well in an isotropic medium is solved by the method of superposition in which the solution of two simple flow fields are superimposed. The first field consists of flow from a radial line source and the second field is gravity drainage. The potential function for a radial line source is

$$\phi = \frac{Q}{2\pi k} \ln(r) \quad (1)$$

where ϕ is the potential, k is the hydraulic conductivity of the medium, and r is the radial distance from the line source.

The potential field created by gravity may be considered saturated drainage at a unit gradient. It is also assumed to represent the gravity field under conditions where saturated conditions do not occur, but where capillary forces are

dispersance are neglected, therefore, in the gravity drainage scenario, the potential gradient is 1, and

$$\frac{\partial \Phi}{\partial r} = 1 \quad , \quad \frac{\partial \Phi}{\partial z} = 0 \quad (2-9)$$

The solution for the potential function for the case of gravity drainage may therefore be written as

$$\Phi = r \quad (2-10)$$

The two flow scenarios may be combined using the method of superposition. The variable r is converted to anisotropic coordinates ($r^2 = x^2 + y^2$):

$$\Phi = -\frac{g_0}{2\pi k} \ln(\sqrt{x^2 + y^2}) + r \quad (2-11)$$

A stagnation point occurs at $V_{\text{max}} = 0$. At this point, a singularity of zero flow develops where the potential gradient in the vertical direction is zero. The value of r_{max} may therefore be determined by solving Eqs. 2-4 when $\theta = 0$, and $\partial \Phi / \partial y = 0$. This results in

$$r_{\text{max}} = \frac{g_0}{2\pi k} \quad (2-12)$$

The nonphysical function of the potential function is the stream function, which describes the flow path of fluid particles from the injection well. The stream function, say

be eliminated from Eq. 3-10 which results in the relationship

$$\psi = \frac{\partial \phi}{\partial r} dr \quad 3-11$$

such that,

$$\psi = -\frac{1}{\rho \nu \mu} \tan^{-1} (\frac{y}{r}) + \delta \quad 3-12$$

The boundary for the saturated bulb occurs where $\psi = 0$, and this relationship may therefore be determined as

$$\frac{y}{r} = \tan \left(\frac{\pi \nu \mu \delta}{\rho} \right) \quad 3-13$$

The value of y_{sat} may be determined by substituting Eqs. 3-8 for conditions when y approaches ∞ :

$$y_{\text{sat}} = \frac{\delta}{\nu} \quad 3-14$$

From Eqs. 3-13, the value of y_{sat} may be determined at the boundary where $y = 0$:

$$y_{\text{sat}} = \frac{\delta}{\nu} \quad 3-15$$

In an isotropic medium, the stress lines will be perpendicular to the lines of equal potential. An example flow net for the saturated flow conditions surrounding the saturated boundary unit is presented in Figure 3-2.

3.2.1. ANISOTROPIC MEDIUM

Often it is necessary to account for anisotropic conditions in a porous medium. This is especially true in

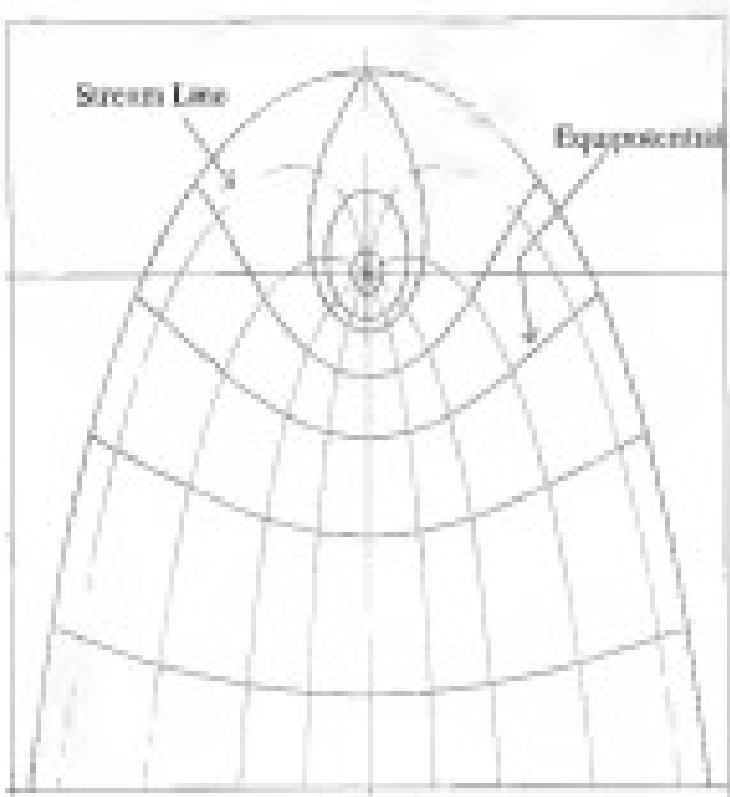


Figure 2-2. Equipotential and Stream Lines resulting from a horizontal injection well.

solutions which involve the flow of water in both the vertical and horizontal directions. Many times the measured value, hydraulic conductivity in the horizontal direction will be greater than in the vertical direction as result of the manner in which sediments are deposited over time. This situation occurs in a landfill where waste is deposited and compacted in horizontal layers. Specimens for the saturated zone surrounding a horizontal injection well in an anisotropic medium may be developed using the same method as the isotropic case. It is assumed the material is homogeneous and that anisotropy corresponds to the principal axes of the system. The governing equation for the case of steady plane flow is

$$\kappa_x \frac{\partial^2 \phi}{\partial x^2} + \kappa_y \frac{\partial^2 \phi}{\partial y^2} = 0 \quad 2-11$$

where κ_x and κ_y are the hydraulic conductivities in the x and y direction, respectively. The anisotropic problem may be solved by means of an equivalent isotropic flow region by an appropriate angle change. The method has been previously utilized by Bear and Dagan (1984). The solution of the potential function for a line source in an anisotropic medium using the method of an equivalent isotropic flow region was presented by Carlier and Dagan (1986). When combined with Eq. 10 by the method of superposition, the resulting potential function for an injection well in an anisotropic medium is

$$\theta = \frac{Q}{4\pi k T_c L_p} \ln \left(\frac{L_p^2}{L_0^2} + \frac{L_0^2}{L_p^2} \right) + \phi \quad (2-12)$$

Using the same techniques applied in the isotropic case, the equation of the saturated zone may be determined as

$$x = \frac{R}{T C_p} \tan^{-1} \left(\frac{R}{P_1} \sqrt{\frac{k_1}{k_0}} \right) \quad (2-13)$$

The parameters T_{sat} , k_{sat} , and x_{sat} may be determined as

$$T_{sat} = \frac{Q}{2\pi k T_c L_p} \quad (2-14)$$

$$k_{sat} = \frac{R}{L_p} \quad (2-15)$$

$$x_{sat} = \frac{R}{L_p} \quad (2-16)$$

The distances x_{sat} and k_{sat} are a function of the hydraulic conductivity in the vertical direction only. The location of the unsaturated zone above the well, T_{sat} , is function of hydraulic conductivity in the vertical and horizontal directions, and thus varies for differing degrees of anisotropy. The effect of the degree of anisotropy on the shape of the saturated bulb is illustrated in figure 2-3.

Injection flow and pressure relationship

In cylindrical geometry of interest is a horizontal injection well system so the injection pressure required for a given flow rate is a given set of media conditions. The

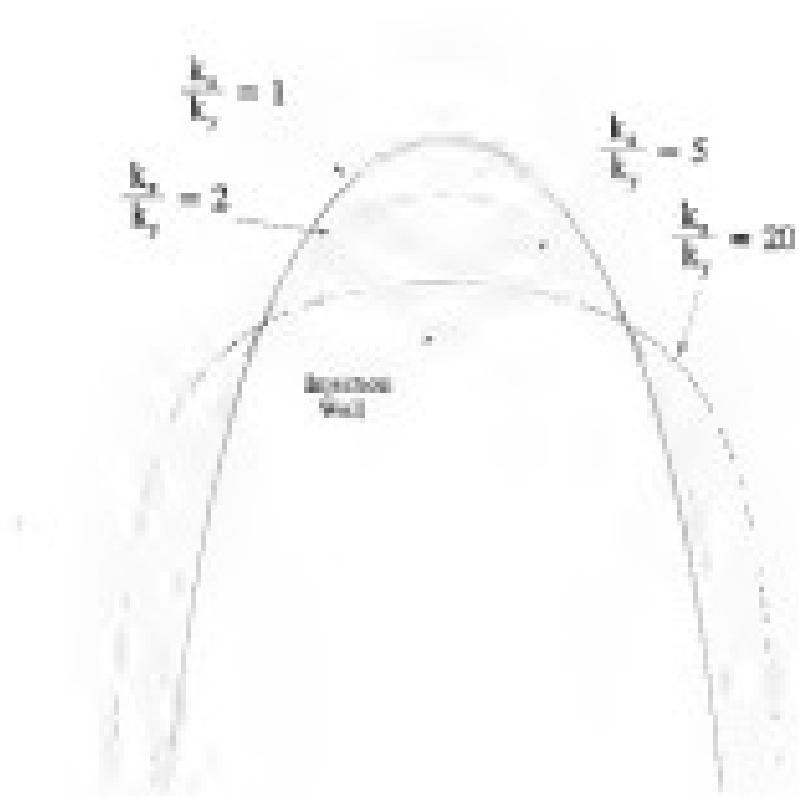


Figure 3-3. Effect of Anisotropy on Boundary Layer

pressure head required, P_0 , may be defined for isotropic conditions as

$$P_0 = -\frac{\partial}{\partial z} \ln \frac{F_0}{F_\infty} \quad (2-17)$$

and for anisotropic conditions as

$$P_0 = \frac{\partial}{\partial z} \ln \frac{F_0}{F_\infty} \quad (2-18)$$

where r_0 is the effective well radius and R is the radius of influence of the line source. In the anisotropic relationship for a line source, the radius of influence increases upwards towards infinity. It is therefore necessary to assess some radius at which the effect of the line source is negligible. In the case of a horizontal injection well, this may be viewed as the distance beneath the well at which the effect of the well is no longer observed. The radius of influence may be estimated in the same manner as typical well hydraulics using empirical or semi-empirical estimates (Bear 1979). These estimates often vary widely and P_0 should be evaluated over a range of R values.

Isotopic flow to the LCR

The flow of isotopes into the landfill bottom drainage layer is a critical part of the design of the leachate collection system (LCR). If the LCR was located at an infinite distance beneath an injective line, then the flow into the LCR would be equal to the injected flow rate.

however, the closer the net is located to the injection line, the greater the flow rate per unit area. The flow rate for a given area of the flow net may be determined from the difference between the excess fracture lines, which may be estimated using Eqs. (47),

Discussion

The steady state equations presented here allow an estimation of the shape of the saturated flow zone that results from a horizontal injection well in a fracture which is treated by a LSC. Despite presenting the change in T_{sat} , θ_{sat} , and P_0 as a function of the linear flow rate and the fracture conductivity are presented in Figures 3(a), 3(b), and 3(c) respectively.

The greatest limitation to the application of this analysis is the neglect of unsaturated flow conditions. Unsaturated flow does occur in a fracture, and is the predominant means of moisture transport for low saturation flow conditions. In the case of a horizontal injection well under pressure at steady state, the force of pressure and gravity will be the dominant transports methods in the area immediately above the walls. A loss of moisture transport will occur in the area immediately below the saturated zone as a result of capillary forces, and may affect the shape of the zone. At larger pressures, the potential created by hydrostatic pressure should be much greater than the capillary potential.

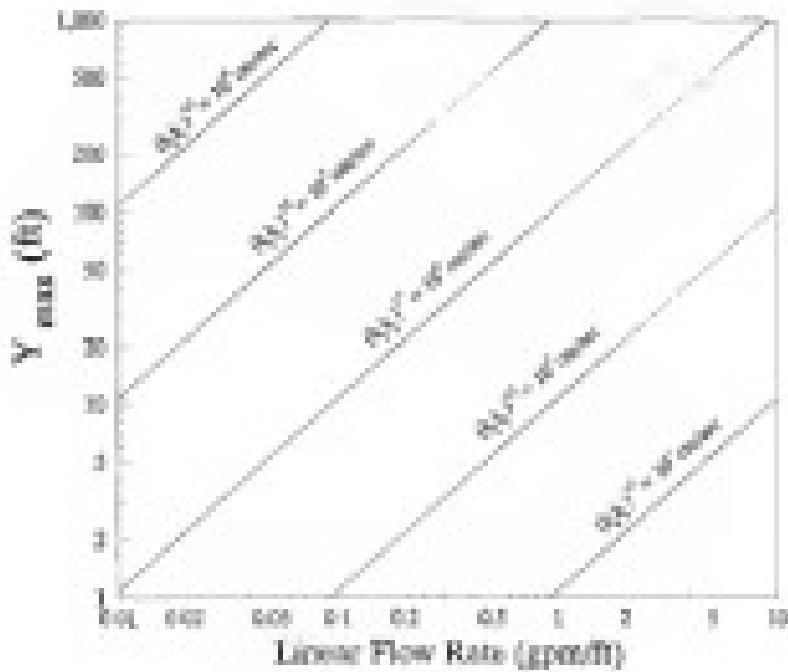


Figure 2-4: τ_{max} as a Function of Linear Flow Rate

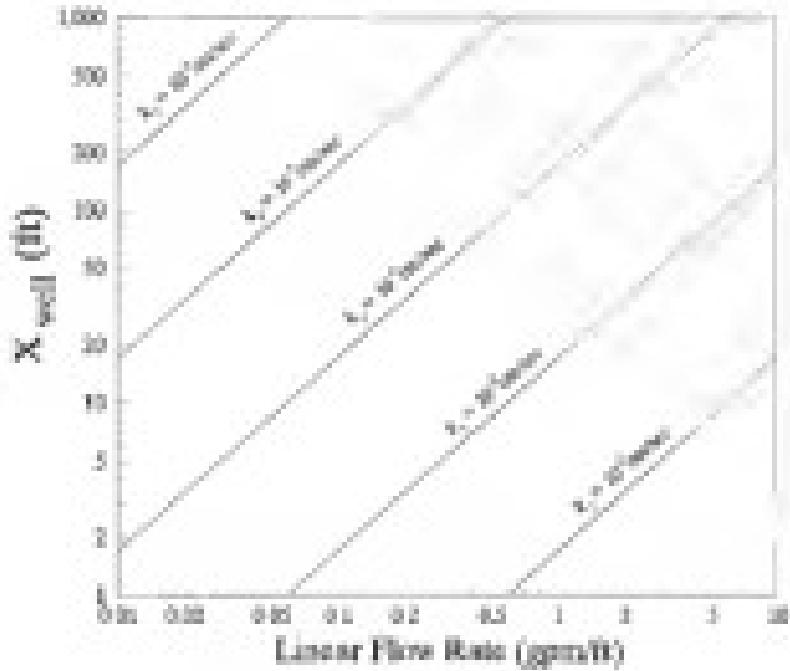


Figure 2-9. K_{well} as a Function of Linear Flow Rate

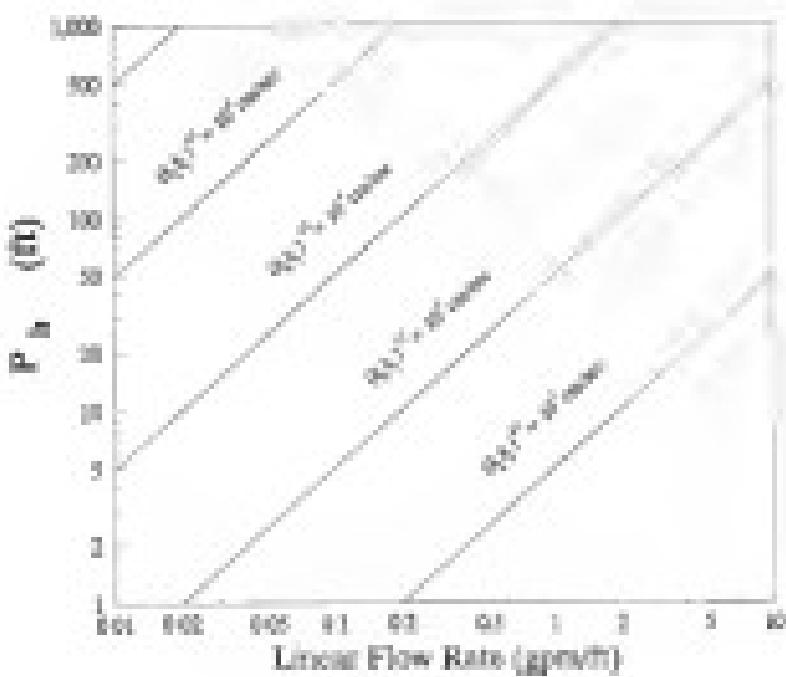


Figure 3-8. Pressure Head as a Function of Linear Flow Rate ($Re_e = 1000$)

The above equations were developed to allow design under assumed flow conditions which might be encountered in SO-CO₂ operation. For example, injection into the CO₂ will be at a minimum when a saturated zone develops surrounding an injection well and reaches into the CO₂. Although planned CO₂ operations may not reach steady state, the maximum possible conditions should be designed for to accommodate future operating conditions.

Conclusion

Equations were developed to describe the shape of the saturated zone surrounding a horizontal injection well under steady-state conditions. The injection well was treated as a line source subjected to a gravity drainage flow field, and capillary forces and dispersion were neglected. Solutions were presented for isotropic and anisotropic cases. The predominant driving forces of water movement were assumed to be the pressure of the injected water and gravity. The method of analysis outlined here is proposed as a method to establish design criteria for the application of a SO-CO₂ in full-scale injectables. The equations allow a user to design injection well spacing, and the depth into the surface at a given flow rate. An estimate of the pressure head, which is necessary to properly run the pump and piping system, can be obtained as well.

CHAPTER 3
LEACHATE RECYCLE UNDER MONITORING CONDITIONS
AT A FLORIDA LANDFILL

Introduction

Leachate recycle involves the recirculation of leachate collected from a land landfill back through the landfilled waste. This practice provides leachate volume management and offers the potential to accelerate the decomposition of biodegradable waste in a landfill. Leachate recycle has been successfully demonstrated in pilot-scale studies to enhance waste stabilization (Jacob et al. 1979; Pohland 1989), and has been practiced at a number of full-scale landfills with some positive results (Rutherford and Meek 1994).

The recycle of leachate to a landfill may be performed by a number of methods including spray irrigation, surface application, and direct recharge to the interior of the landfill. Vertical recharge wells have been utilized to recycle leachate, but the resulting circulation of solutes through the waste is questionable. Horizontal injection wells offer the potential to distribute solutes over large areas of a landfill, while avoiding the problems associated with leachate exposure to the environment such as migration of odor and methane. Horizontal injection wells minimize

interference with normal landfill operations and vehicle and equipment traffic. The concept of injecting through horizontal distribution systems has been briefly mentioned by other writers (Bertoldi and Anderson 1990), but no detailed study of their construction and performance has been reported.

This paper presents the results of a horizontal injection leachate composite system (HILS) at a lined landfill in Florida. The construction, operation, and performance of eleven injection lines are reported for a period from February, 1990 through August, 1994. The information is presented to facilitate the use of this technology at other landfills sites, and provides information relevant to the construction and operation of HILS and the design of such systems. The effect of the HILS on a number of additional landfill processes, including leachate generation and composition, waste decomposition, landfill temperature, and gas production, were monitored at this landfill site, and will be reported elsewhere.

Methods

Site Description

The horizontal injection leachate composite study was performed at the Marion County Southwest Landfill (previously known as Central Florida) (figure 2-1). The 37-acre (15-hectare) landfill is lined with a composite liner and is equipped with a leachate collection and removal system. Leachate design

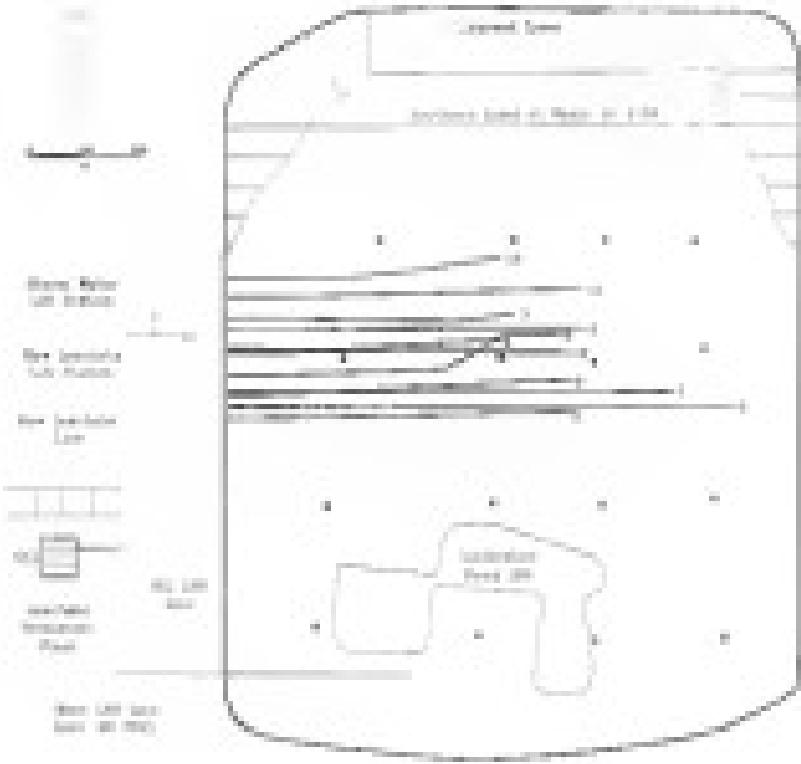


Figure 3-1. Plan View of ACME with Infrastructure Lines

from the landfill to a lift-station and be pumped to a leachate equalization-treatment plant. The landfill includes an infiltration and filter-precipitation leachate treatment system treated leachate is treated off-site for disposal at a waste water treatment plant. An infiltration pond leachate recycle system (ILRS) was operated beginning in 1988 (Gossen et al., 1990) prior to the part of a project involving the accelerated stabilization of the stabilized waste (Gossen et al., 1990) by:

The site receives an average of 80 inches of rain annually. Approximately 100 tons per day of waste were deposited in the lined landfill until at the time of this research. Apparent waste composition is approximately 18% to 19% dry/yr². Cover soil consists of sand mixed on site. Waste is deposited in a set of four lifts which are placed in an east-west fashion and which slope upward to the south against the previous set of lifts.

ILRS Construction.

The construction of three initial injection lines began in December 1991 on a series of four lifts constructed north of the infiltration pond area. These injection lines were placed in this series of lifts, the first on top of lift 1, the second on top of lift 2, and the third on top of lift 3. The result was a stepped configuration in which the three injection lines were the northwestern and positioned at the lowest elevation, and the third injection line was the

southermost and at the highest elevation. Upon completion of one set of injection lines, another set of three lines was placed in the next series of bents in a similar fashion. The resulting lines installed is shown in Figure 3-3, displaying the position of the injection lines in place at the end of August 1974, eleven of which were used and discussed here.

The characteristics of each RIL are listed in Table 3-1; the length and location of each injection line was dependent on the available area of bents. The design pipe diameter for the concrete recycle piping system was 3-inches, and this diameter was used for the injection lines as well. Holes were drilled in the injection pipe before installation. The hole size and spacing in the original injection line were designed to distribute flow evenly throughout the trench. It was felt that continuous by injected concrete would soon likely penetrate the soil mass surrounding the trench, and the trench would fill with concrete under pressure, preventing the need for distributed flow from the pipe. The new injection lines (RILs 3-11) were therefore not designed with additional holes to accommodate for potential clogging and plugging.

PVC pipe was selected for the majority of the injection lines because of ease and quickness of installation. The PVC pipe was utilized with success during installation. A high density polyethylene pipe was installed for RIL 7 and was fluorocarbonized prior to installation. The length of each injection line placed was dictated by the length of individual

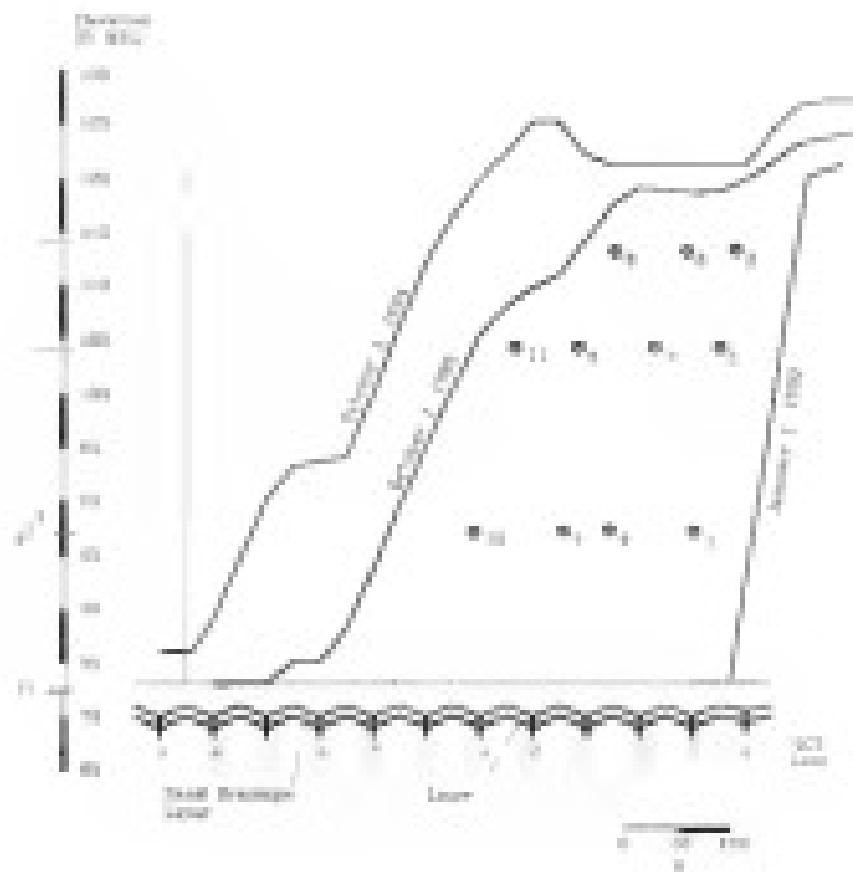


Figure 3-3. Cross section of tapering zones

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“I am afraid, James, we've had a bit of trouble,” said Mr. Trelawny, “but our slaves are very good.”

sites at the time of installation. Injection lines 1 and 2 were constructed to cross the entire bottom length of the landfill (150 ft and 100 ft, respectively). This necessitated building the lines in phases because the entire lift lengths were not constructed during one site visit. The process of phased construction required precise coordination of waste placement and repositioning of part of the trench. To minimize these difficulties, the remaining injection lines were constructed in one phase, utilizing the depth of 100 ft available.

Construction of the injection trenches for lines 3 through 11 were completed with a backhoe, which was used to excavate a trench down the center of the 20 ft wide waste area. The trench for RIL 1 was constructed using a bulldozer, which resulted in a much larger trench volume. The backhoe trenches were approximately three feet square, and the excavated waste and cover material were placed to the side of the trench. Blasted lime was used as drainage material in injection lines 1 through 8. The lime was placed at the bottom of the trench to a depth of approximately 1 foot. Lime was not placed in lines 9 and 11 for comparison of injection performance.

The pipe was placed in the trench and glued. An additional eye to the bottom of cracked tiles (10 mm) was placed on top of the pipe and spread evenly. The terminal end of the pipe was capped. Non-puddled pipe was installed in

the dikes at 1 ft of breach and no time were placed in this area of the breach to prevent channelling along the pipe. This trench area was covered only with mats. The injection lines were connected to non-penetrated river pipes up the side slope of the breach. The injection line area of the breach was covered with uncoated mats and compacted using a progression of equipment, from light to heavy. An effort was made to keep the trenches covered on all sides with mats, and not covered, which could lead to short circuiting of injected densities.

Benthic injection lines were connected to a main line manifold line which ran along the seepage area (initially) to the DIP and two submersible discharge and well pumps (2 hp and 3 hp) in the raw treated aquiferous barge. Each DIP was linked separately to allow injection into any desired interval. The pumps were valued to allow independent and parallel operation.

System operation and monitoring

The parameters were selected to assess the hydraulic performance of the system, benthic flow and pressure. Flow was measured using a positive-displacement water transducer (analog output) installed in the main manifold line on the barge. Pressure was measured with an analog output pressure transducer located in the manifold line on the barge 30 ft before the first DIP. Analog signals were recorded by

data loggers in the field which were periodically downloaded to a portable computer.

Injection Schedule

The application of lauobate to surface injection lines, and the frequency and rate of application, were dictated by a number of factors. These factors included research goals of monitoring the effect of the TMI on the landfill system, the volume of water available for injection, and the schedules of the landfill operating crew. The injection of lauobate was suspended at times to allow the landfill system to be maintained and for the repair and maintenance of the RT-200. All of the injection sites reported here involved lauobate recycling into one injection line at a time.

Initial injection tests were conducted during February through April 1993, using injection lines 1 and 2. During the initial test period, lauobate was injected for prolonged periods to observe the physical operating characteristics of the system. The next round of injection tests began in September 1993, and from that time lauobate was injected on a daily basis, at a rate of 60,000 gallons per day. This flow rate is an arbitrary level established by the landfill's permitting authority. The schedule of injection during the period from September 1993 to January 1994 consisted of rotating injections onto lines 1 through 6 at approximately 60,000 gallons per day for two or three days into each line. In the spring and summer of 1994, lauobate injection began into lines 7, 8, 9,

10, and 11, which contained limited injection into holes 1 through 4.

Results and Discussion

III. Construction

Construction of the R-100 was performed by leadline injection using typical leadline equipment. The most noticeable difficulties encountered in RIL construction were timing of RIL construction and slope resulting from unexcavated waste. Because the injection lines were constructed within 100 ft of waste, the available construction time was often only a matter of days. This was especially true in the cases where the end point of the lower lift, the beginning point of the upper lift, and the inlet section of an RIL coincided. In these cases, RILs were often constructed in the presence of other leadline sections. The location of the trench on the surface of the hillside was determined by considering the location of the bedrock mass, the proximity to large overburden layers, the proximity to vertical gas wells, and the slope available for the backhoe to excavate the waste. Although a rubber-tired backhoe was used at RSWL, a backhoe or truck would have allowed more flexibility for RIL placement in areas of steeper slopes.

The trenches were excavated in a manner designed to avoid direct contact with thick layers of cover material which could result in start-sinking. Complete enclosure of these layers was impossible. Covering the trench with solid waste

and supervising the areas where the tanks required connection. Instruction of the hauler operator to ensure sufficient waste was on top of the line before heavy equipment was used. The shredded tires did act as adequate bedding and cover for the pipe in this process.

Also presented a problem were bridge areas of Hydril were left open for periods of time greater than 12 hours. This was corrected by backfilling the arched material and pipe during or immediately after trench excavation in such a manner as to ensure that no trench area was left open more than 12 hours.

The injection lines were checked for integrity prior to use. All the first 12 injection lines, two were found to be deteriorated. These RIC were each in the upper level and in the non-perturbed pipe section. This area of the injection system was most vulnerable to damage from vehicles and heavy equipment because of the proximity of the pipe to the hauler surface and access roads. Injection lines on the lower levels were generally covered with large thicknesses of waste soon after completion, and traffic was on a profile for these. The proximity to the surface, did however, permit separation and repair of damaged pipe sections. The deteriorations were the result of harsh equipment or trucks crossing pipe and both sourced near the major access road for solid waste delivery vehicles. After the initial spring 1999 test period, a blowdown was conducted to RIC 3 at 400 ft during the construction of a temporary park.

While a detailed analysis of the structures used in the RCL construction was not performed by this study, it should be considered in the design of such a system. The presence of transverse equipment and the occurrence of differential settlement creates conditions that can cause pipe breaks. Differential settlement presents the greatest risk to pipe breaks in lines constructed over large thicknesses of waste. The greatest concern of ADWW was a break in the pipe in the bedrock covered clay section, because such a break would result in loss of use of that line. A pipe break in the perforated section of the pipe presented less of a concern to the RCL since used absorbent drainage material. In the event of a break, the lines would still allow some hydraulic transmission.

Bedfill equipment did result in stress at the piping connections of the RCL and the RCL manifold. This resulted in some loss in valves and connection. Future construction should include flexible hose connections to replace any rigid connections between pipes inside the bedfill and pipes outside the bedfill.

Leachate Pumping Test Data

A total of 1,000,000 gallons of leachate were recycled using the RCLPP during the period from February 1993 to August 1994. The total volume of leachate injected into each

Table 3.3. INVESTIGATION REPORTS EXAMPLE

| NO. | Start Investigation | Total number of Investigations | Total Volume (in mbars) |
|--------------|------------------------|--------------------------------------|-------------------------------|
| 1 | Feb 4, '93 | 323.3 | 2,314,380 |
| 2 | Mar 22, '93 | 388.3 | 2,327,180 |
| 3 | May 16, '93 | 34.4 | 276,820 |
| 4 | Sept 12, '93 | 172.6 | 168,820 |
| 5 | Dec 1, '93 | 182.8 | 168,820 |
| 6 | May 27, '94 | 41.3 | 263,320 |
| 7 | Mar 3, '94 | 223.3 | 1,254,480 |
| 8 | May 4, '94 | 123.3 | 824,320 |
| 9 | June 8, '94 | 31.3 | 136,320 |
| 10 | July 6, '94 | 57.3 | 146,320 |
| 11 | July 18, '94 | 53.3 | 138,320 |
| Total | — | 1,718.4 | 2,914,180 |

line during this period is presented in Table 3-2. The greatest volume of leachate was injected into RIL 1, primarily as a result of the initial injection period in the spring of 1993. As a result of the length of this line, and the large trench volume, the initial conditions offered little resistance to flow. Overall, greater volumes of leachate were injected to RIL constructed on the lower and middle 15ft relative to RIL on the top 15ft. The operation of the injection system in these upper 15ft resulted in occasional surface sprays on the flow lines and pressure created by the leachate storage pump. The spray caused an pellet clog in the outlet and (lack of the perforated pipe section), and resulted from water flowing through non-conductive soil material or channels caused by porous sugar beetage.

Flow/Pump Relationship:

The resultant flow rates and pressures to the main sections were recorded for each injection run. A typical flow and pressure response occurring during an injection period is presented in Figure 3-3. The flow rate started at the highest value, and decreased towards a steady state. The pressure started at a low value and tended towards a higher steady value. The slight decrease in pressure at steady state conditions was the result of dropping headloss losses in the leachate storage tanks. The degree of this change and the time to reach a steady value were a function of the volume of leachate previously injected, the degree of saturation,

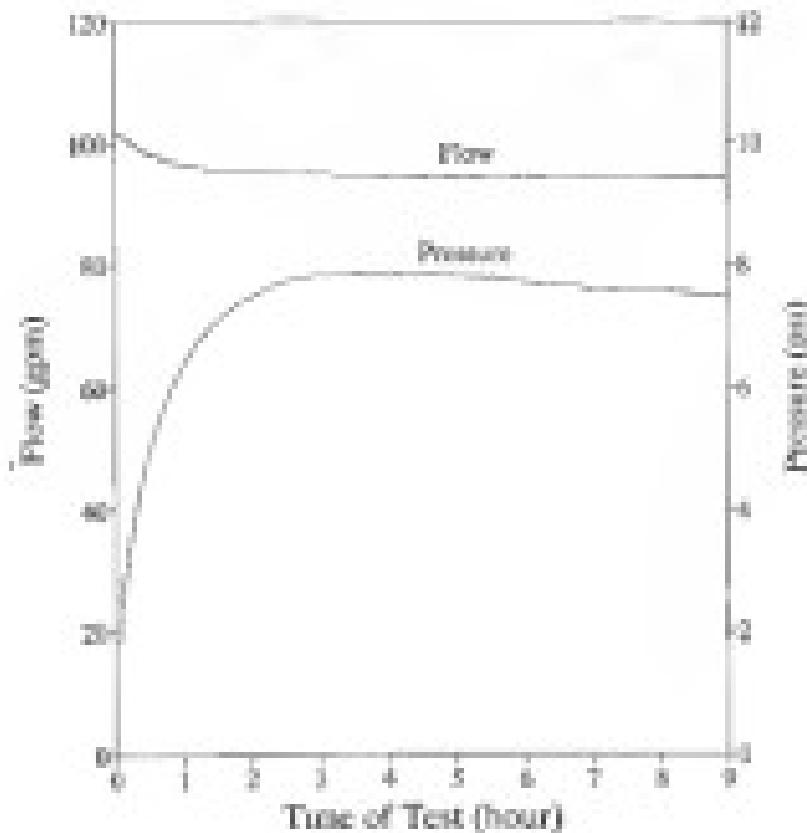


Figure 3-3. Typical injection flow and pressure response

flowing from any nearby irrigation lines, and the total storage volume in the trench.

The backhoe flow and pressure responses were recorded for each TIL as a function of calendar time and cumulative pumping time, and those results are presented in Appendix A. To better understand the TIL length and to estimate the actual applied pressure at the inlet of the perforated section of an TIL, flow and pressure at the metering point were converted to linear flow rate (cusecs per foot of injection line), and applied pressure head (feet of water column). The applied pressure was estimated from the pressure recorded in the line at the pressure gage, the average diameter of the line, and expected head loss from the pressure gage to the air inlet. Figure 10 presents the linear flow rate and applied pressure head for TIL 1, a line which received a total of 0.3 million gallons of recycled wastewater. The data are presented as an average of 0.1 day time increments. The pattern of decreasing flow and increasing pressure at later time periods was observed in the long term trend results as well. The results are presented in Appendix A for each TIL.

The flow rate which occurs at a given applied pressure provides information regarding the performance of the system, its change over time, and is data needed for the design of similar systems. A parameter is defined to represent the ratio of linear flow rate (cusecs) to the applied pressure head at the inlet of a TIL (ft. w.c.).

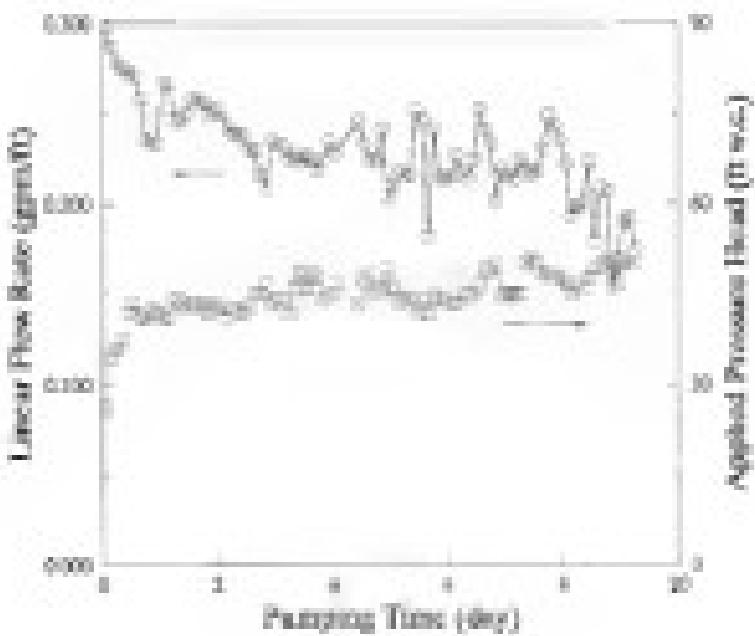


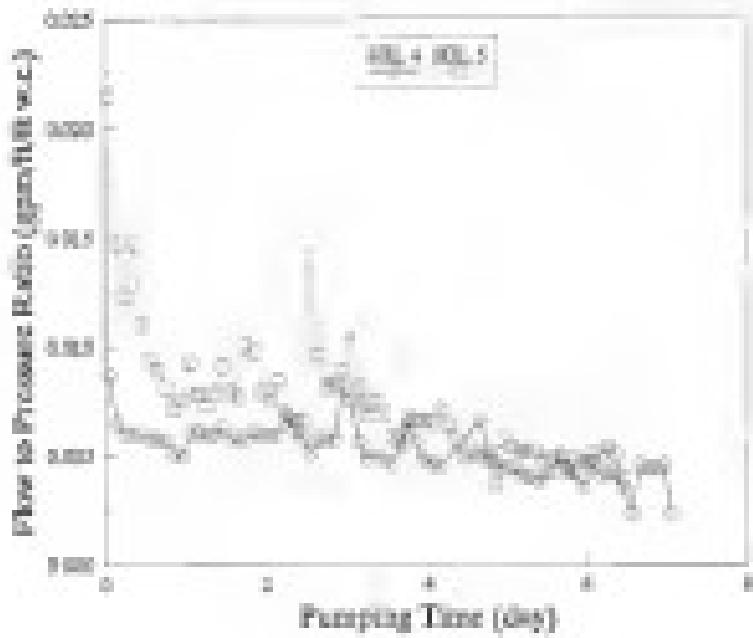
Figure 3-4. Linear Flow Rate and applied Pressure Head versus Time. SIC-7

Table 3.3. Average Injection Flow Rates and Applied Pressures

| STL | Flow Rate (gpm) | Average Inj. Flow Rate (gpm/100) | Average Applied Pressure Head (ft. water) | Average Doppler (gpm/ft.100) |
|-----|--------------------|---|---|------------------------------------|
| 0 | 79.0 | 0.129 | 45.3 | 0.00040 |
| 0 | 73.0 | 0.102 | 35.6 | 0.00030 |
| 0 | 64.0 | 0.107 | 35.7 | 0.00030 |
| 0 | 77.4 | 0.118 | 41.0 | 0.00034 |
| 0 | 88.3 | 0.108 | 35.7 | 0.00030 |
| 0 | 78.4 | 0.142 | 35.8 | 0.00030 |
| 0 | 78.0 | 0.121 | 45.4 | 0.00040 |
| 0 | 77.0 | 0.140 | 35.8 | 0.00034 |
| 0 | 72.4 | 0.124 | 35.8 | 0.00031 |
| 10 | 72.0 | 0.100 | 45.0 | 0.00041 |
| 11 | 49.0 | 0.100 | 35.3 | 0.00040 |

The average results of flow rate, linear flow rate, applied pressure head, and α , are presented in table 2-3 for each RIL. The results represent averages for the entire period of injection, with exception of RIL 1 and 3, which do not include the data from the spring 1993 test. While a large volume of leachate was recirculating during the spring 1993 test, a number of the data files were lost, and only one pump was installed during this time. Thus pump clogging was observed which proved to provide erratic results in regard to the pressure and flow data (see Appendix A). The value of α as a function of cumulative pumping time is presented in Figure 2-1 for RIL 4 and 5, Figure 2-2 for RIL 1 and 3, and Figure 2-3 for RIL 6, 8, 10, and 11.

A number of observations were made regarding the pattern of α as a function of time. The RIL sites resulted in the greatest measured flow to pressure response were those nearest the landfill surface. These were the sites in which the infiltration of surface springs was the greatest. Two factors likely played a role in this phenomena. First, it was realized that the hydraulic conductivity was greater in this area because of smaller effective stress resulting from smaller depths of waste above these injection lines. In addition, the large pressures which occurred in the injection system at ACTM created upward waste uplift conditions so that the force of the injected leachate could create preferential channels. During injection into a surface RIL,



Figures 3-4. a) response times: RIL 4 and 5

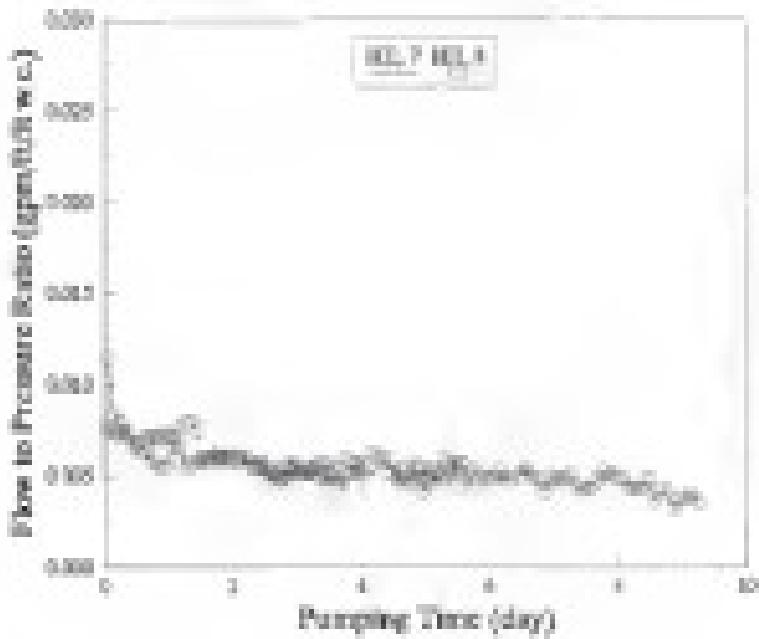


Figure 3-5. a. Vertical Boxes HCL 7 and 8

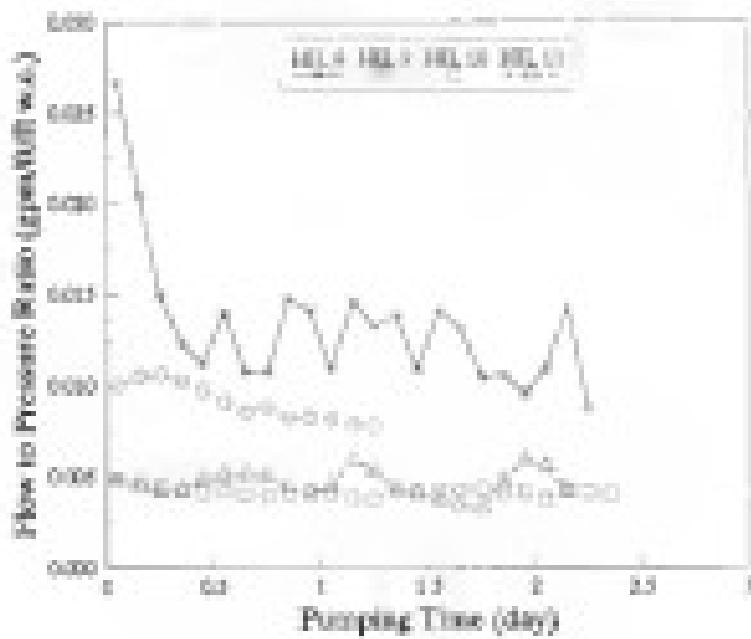


Figure 3-17. π versus time - Fig. 4.7.30.31.

Institute injection was observed to visibly split a limestone root with the discharge of a surface spray. The results in the upper hills were the most variable because of the phenomena and because these hills were operated by a very intermittent pump.

It was previously observed with the flow and pressure relationships over time, the cause of a decreased water line as opposed to air for all the hills. A number of potential reasons may be cited to account for this. The reduced reduction in flow response was a result of the saturation of the surrounding waste and truck, and the filling of the available storage volume. A potential cause for long term reductions is the occurrence of clogging or sealing of the penetration in the pipe, and the truck itself. Another possibility which was visibly observed at the landfill was the back pressure of landfill gas in the injection lines. At times after an injection run, gas pressure as high as 100 inches of water column was recorded. The higher gas pressure, which could result from increased gas production and reduced void space in the unsaturated waste, would result in reduced relative permeability for water flow through the solid waste. To accommodate long term flow reduction, the ability to operate at higher pressures, and the ability to extract gas should be considered as part of system design.

The most representative flow response for the injection lines was observed in Hill 4, 5, 7, 8, 10, and 11. These

lines were buried deep enough in the landfill to avoid surface seepage problems. The average α value is lines 4, 5, 7 and 8 ranged from 0.0031 to 0.0045 gpm/ft²/ft w.e., the average α values for lines 10 and 11 per line stratum separately were 0.0031 and 0.0044 gpm/ft²/ft w.e.. The injection system without valves still functioned, although at slightly lower pressures. Construction without lines made the installation process much easier and more rapid for the operator, but a pipe break in one of these branches would greatly reduce injection performance.

The range of values presented above represent the most applied conditions at ACME as measured during the injection experiments and the ones which should provide the best reference for the design of similar systems. It should be noted that the α values measured were for a specific flow range and extrapolation beyond this flow range may provide incorrect results. Future tests at the ACME RI-100 should include the performance of injection tests at lower flow rates for prolonged periods of time to measure the steady state response of the system.

Reinforced Conductivity Definition

In a previous chapter (chapter 3), an equation was presented which related the injection pressure to flow rate for a horizontal well based on the storage hydraulics, such that:

$$R_s = \frac{q_{inj} \ln(\frac{R}{r_0})}{2\pi k_x k_y r_0} \quad (3-1)$$

where q is the linear flow rate, k_x and k_y are the hydraulic conductivities in the x and y directions, r_0 is the radius of influence for the line source solution, and r_0 is the effective radius of the well.

Although the injection tests reported in this paper were not designed to determine the validity of this relationship, the data collected can be used to estimate the magnitude of the hydraulic properties of the matrix. An additional fact that makes this analysis useful is that previous tests were conducted in the same fissure using an infiltration pool test. The vertical hydraulic conductivity, k_z , was estimated from those experiments as 1000 m yr⁻¹ by *et al.* (1988). The injection test data can therefore provide some estimate of the degree of anisotropy. The infiltration pool tests were performed on an area much of the 30-320. Supplementary borings in the two areas suggest that the matrix conductivity was greater in the pool areas than in the injection areas.

The difficulty associated in the use of a line source solution is the necessity to assume a value for the radius of influence. Table 3-6 presents hydraulic conductivity estimates for the four representations (Eqs. (4,5,7,8)) for values of R/R_0 of 100 and 1000. Hydraulic conductivity estimates are made for no anisotropic assumption, and the anisotropic assumption with k_z values of 4000 m yr⁻¹ and

Table 3.4. Hydraulic Conductivity Estimates

| R_s | K ($\text{mm}/(\text{Pa}/\text{hr})$) | R_s/r_s | K_s ($\text{mm}/(\text{sec})$) | K_c ($\text{mm}/(\text{sec})$) |
|-------|--|-----------|---------------------------------------|---------------------------------------|
| 4 | 1,000.00 | 1.00 | 2.00×10^{-4} | 2.00×10^{-4} |
| | | 1.00 | 1.00×10^{-4} | 1.00×10^{-4} |
| | | 1.00 | 4.00×10^{-5} | 1.44×10^{-5} |
| | | 1.00 | 2.00×10^{-4} | 0.97×10^{-4} |
| | | 1.00 | 1.00×10^{-4} | 0.49×10^{-4} |
| | | 1.00 | 4.00×10^{-5} | 0.19×10^{-4} |
| | | 1.00 | 2.00×10^{-4} | 0.10×10^{-4} |
| 5 | 0,000.00 | 1.00 | 1.40×10^{-4} | 1.40×10^{-4} |
| | | 1.00 | 0.70×10^{-4} | 0.70×10^{-4} |
| | | 1.00 | 0.40×10^{-4} | 0.40×10^{-4} |
| | | 1.00 | 0.14×10^{-4} | 0.14×10^{-4} |
| | | 1.00 | 0.06×10^{-4} | 0.06×10^{-4} |
| | | 1.00 | 0.04×10^{-4} | 0.04×10^{-4} |
| | | 1.00 | 0.02×10^{-4} | 0.02×10^{-4} |
| 7 | 0.000.00 | 1.00 | 2.00×10^{-4} | 2.00×10^{-4} |
| | | 1.00 | 1.00×10^{-4} | 1.00×10^{-4} |
| | | 1.00 | 4.00×10^{-5} | 1.44×10^{-5} |
| | | 1.00 | 2.00×10^{-4} | 0.97×10^{-4} |
| | | 1.00 | 1.00×10^{-4} | 0.49×10^{-4} |
| | | 1.00 | 4.00×10^{-5} | 0.19×10^{-4} |
| | | 1.00 | 2.00×10^{-4} | 0.10×10^{-4} |
| 8 | 0.000.00 | 1.00 | 0.90×10^{-4} | 0.90×10^{-4} |
| | | 1.00 | 0.45×10^{-4} | 0.45×10^{-4} |
| | | 1.00 | 0.18×10^{-4} | 0.18×10^{-4} |
| | | 1.00 | 0.06×10^{-4} | 0.06×10^{-4} |
| | | 1.00 | 0.03×10^{-4} | 0.03×10^{-4} |
| | | 1.00 | 0.01×10^{-4} | 0.01×10^{-4} |
| | | 1.00 | 0.005×10^{-4} | 0.005×10^{-4} |

1000³ cu/yds. The mobilized hydraulic conductivity ($K_{H_2O}/^{1/2}$) were found to be more than one order of magnitude greater than the previous K_H estimates, indicating a decisive electroosmotic nature of the landfill material. The electroosmotic effect would result from the composition of the waste, the manner in which the waste was deposited and compacted, and the presence of sandy coarse soil layers.

Summary and conclusions

A horizontal injection leaching recycle system was successfully operated at a lined landfill in Florida. The data reported here included the construction and operation experiences, and the hydraulic performance of the HLLS. Over a 10-month period, 7,450,000 gallons of leachate were recycled into the injection lines. Construction of the lines was performed by landfill operators with typical landfill equipment.

Applied injection pressure and leachate flow rates were monitored throughout all of the injection tests. The flow rate to applied pressure ratio was monitored, and decreased with time. Potential causes for this observation were clogging of injection lines and fractures, and the large pressure-gain-pressure loss observed in the lines. Substantial volumes of leachate could still be recycled to the landfill at later times. Long term monitoring is needed to determine effects on flow rates after extended operation times. Typical values of flow response ranged from 0.00 to 0.05 cu/yds per

from 0 applied pressure need for trenching with either no drainage material, and ranged from 0.005 to 0.100 for the two RIL without tiles. These values were determined for flow rates ranging from 0.10 to 0.30 qpm/ft. Use of these values for tiles outside this range should be performed with caution until additional data is collected. The results reported here represent the conditions at one location. While favorable conditions may exist site to site, these results provide a starting point for the design of a system.

CHAPTER 4
BIOLOGICAL INJECTION LEACHATE RECYCLE:
CONSTRUCTION-OPERATION GUIDELINES AND DESIGN PROCEDURES

Introduction

This paper outlines guidelines for the design, construction, and operation of biologically-injection leachate recycle systems (BI-LS) at solid waste landfills. Biological injection leachate recycle is a method to reintroduce stabilized landfill leachate back through landfilled material using buried wells buried within the waste. Leachate recycle offers the potential to accelerate the decomposition of biodegradable components in the landfill, to provide an avenue of leachate treatment, and to provide a method of leachate volume management.

The guidelines presented here are the result of three years of work in the construction and operation of a BI-LS at a Florida landfill (Chapter 3) and an analysis of the feasibility of appropriate recycled flow from a biologically-injection well (Chapter 2). The design guidelines presented apply to the sizing and placement of the landfill's hydroseal structures, specifically the DAS pumping and conveyance system, the injection lines, and the leachate collection system. Other landfill aspects not considered here, but which play a potential role in the design of such a system include

the effect of leachate recycle application rates and frequency on the landfill decomposition process, the effect of the RCBG on the overall hydrologic balance at the site, and the utilization of landfill gas from the leaching lines. This chapter provides fundamental information for the implementation of RCBG at solid waste landfills.

Theory of Horizontal Injection

The principles behind the leachate recycle process have been well illustrated in pilot-scale work (Pattie et al., 1979; Polk and 1980) and have been applied at numerous full-scale sites in the United States and throughout the world (Pattie and Anderson 1984; Parker and Marin 1984). A variety of leachate recycle methods have been employed, each with distinct advantages and disadvantages. One method which possesses a number of advantages over other leachate recycle methods is horizontal injection. This technology utilizes perforated pipe or drainage material placed in horizontal trenches buried within the landfill waste. The trenches are constructed during the operational years of the landfill while waste is deposited.

A major benefit the recirculation of leachate to the interior of the landfill without exposure to the atmosphere, allows for injection wells at different locations and allows some control of the rate and frequency of leachate application to areas within the landfill. Buried

Injection wells present unique difficulties with landfill surface operations and vehicle traffic.

Construction and Operation Guidelines

The construction of a RI-LW requires advance planning and timing in regard to the deposition of solid waste. During the process of waste placement, a compacted layer of solid waste is often placed above the base of an injection well immediately after it is constructed; therefore operations must be timed to coordinate with the landfill filling sequence. Construction in the close proximity of landfill vehicular haulage may be necessary and proper safety provisions must be made. The length of time a trench is left open should be limited to reduce soil problems, as well as to comply with regulations regarding the daily application of cover material to solid waste.

The utility of an injection line and spreader as a hydraulic distribution structure should be considered during construction. In a landfill, layers of cover material are distributed throughout, and may act as preferential channels or hydraulic barriers, leading to uneven leachate distribution and surface seepage. Large pressures often develop in the area surrounding a well, and if a layer of highly permeable material undergoes a state of high pressure, a direct snap to the surface, face, or bottom of the landfill may occur. As waste is deposited around an injection well, direct contact with the well cover material should be minimized and RL

should be surrounded by solid waste to the greatest extent possible.

Cover materials with hydraulic properties comparable to solid waste would provide the most uniform solution distribution. The use of an extensive daily cover such as a temporary cap or tarp would create more uniform leachate infiltration conditions, and minimize potential seepage channels. Short cycling may also result from proximity to a gas well. Use of various gas wells in areas of injection should be limited.

Differential settlement of landfilled material should be considered in selecting pipe materials. This is most important for the non-perforated pipe sections connecting the RIL to the LIL pumping system. If a drainage material is provided in the tanks, hydraulic flow would still be possible in the event of a pipe break. Provision must be made to connect the injection lines to a main distribution line along the boundary of the landfill. The ends of the injection trucks should be located a sufficient distance from the landfill face to minimize potential seepage. A clay seal or filter sock should be placed between the perforated distribution and non-perforated connection pipe to prevent preferential flow along the non-perforated pipe. Flexible connections from the RIL to the main distribution line should provide allowances for settlement.

The type of landfill unit also impacts the construction and use of the RI-LAB. Impounded landfills, or landfills surrounded by large earthen berms, are less likely to pose a seepage problem than impervious landfills. Impounded landfills could be operated at greater injection flow rates than impervious landfills. As part of RI-LAB operation, the pressure and flow of the injection system should be monitored routinely during operation. Injections should exist to adjust the rate of landfill flow to maintain performance standards within the design of the system. The landfill should be inspected routinely for seepage that might be the result of the injection system, so that adjustments to the RI-LAB operation can be made.

Design Elements

In the sizing and placement of a RI-LAB, features that must be considered include:

1. Maximizing the distribution of injection throughout the landfill.
 2. Minimizing the potential for leachate seepage to the surface or into slopes of the landfill.
 3. Maintaining the design performance of the leachate collection system in regard to the leachate head above the lines.
- To design a RI-LAB the pipes must be sized and spaced, the dose and frequency of flow application must be forecasted, and the leachate collection system must be designed to accommodate various design leachate recycle rates.

The volume and rate of leachate which will be recycled at a landfill is a function of the landfill's hydrology, topography, and configuration. The factors which play a large role in determining leachate recycle rates include:

1. Total volume of rainfall influencing over the landfill.
2. Volume of stormwater retained within the landfill with which must be treated or leachate.
3. Leachate treatment and disposal capacity within the landfill.
4. Leachate storage capacity at a landfill site.

The latter three factors are determined as part of the landfill design process and should be evaluated in conjunction with the "R-100" design. A hydrologic budget should be prepared which includes the R-100 hydrologic subroutines (Bouyoucos et al., 1964, for example) should be employed to determine design leachate recycle rates.

Injection line spacing

The procedure outlined here for the sizing and spacing of the injection lines, utilizes equations which describe the saturated flow region surrounding a R-100 pumped water pressure (Chapter 3). The equations were developed using a line source saturated flow solution and neglect the effect of capillary potential and dispersion. Under these operating conditions, a horizontal injection leachate recycle system at a landfill

would be operated on an intermittent basis and may not reach steady state conditions. In addition, capillary forces play a role in moisture transport on a timescale (Barfield et al. 1989). However, the method outlined here is not intended as a tool to model moisture production. The intended use of these equations is to estimate threshold design conditions which allow the design of the RI-CLS to perform under conditions of varying design flow.

A schematic of the saturated flow system developed around a RI-CLS is presented in Figure 4-1. The shape of the saturated zone may be described as

$$y = \frac{q}{2k_h} \ln \left(\frac{x}{x_0} \right) \sqrt{\frac{k_h}{k_v}} - \frac{1}{2} \quad (4-1)$$

where q is the linear flow rate, k_v is the vertical hydraulic conductivity, and k_h is the horizontal hydraulic conductivity. The maximum height above the RIC may be described as

$$Y_{max} = \frac{q^2}{2k_h k_v} \quad (4-2)$$

The radius spread of transients may be expressed as

$$R_{max} = \frac{q}{2k_h} \quad (4-3)$$

The lateral distance of transient spread at the well may be described as

$$R_{well} = \frac{q}{2k_h} \quad (4-4)$$

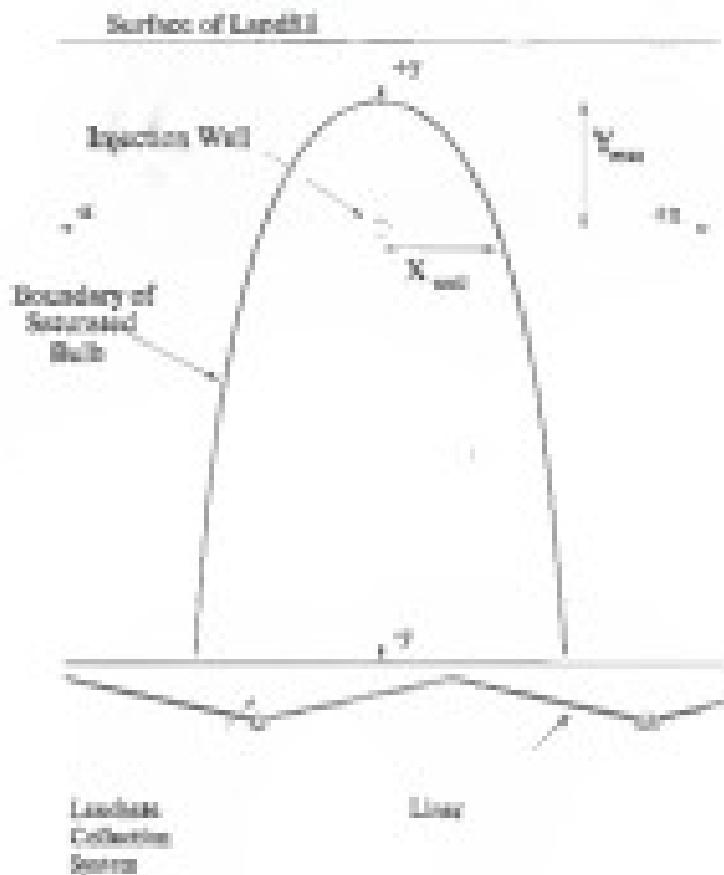


Figure 4-1. Injection Well Flow System

The above equations may be used to calculate the spacing of injection lines to maximize mixture distribution under a given set of operating conditions. Spacing may be based upon estimated zone coverage for average or peak flow conditions. The degree of overlap of zones may be selected by the design engineer based on the engineer's confidence in the design data and the flexibility of the pumping system. An additional distance of 1.0 inches spread which accounts for the unstartled flow zone that would surround the activated zone could be incorporated. The equations can be used to determine locations and operating conditions to minimize the potential for nozzle clogging.

Design of Pumping System

The pressure required to deliver a given flow rate in a specified injection space may be determined by use of empirical data for values of injection flow ratio to applied pressure ratio, defined here as α , determined from other landfill sites. Typical values of α measured at the Alameda County Southeast Landfill (Chapter 1) ranged from 0.018 to 0.001 gpm/lb. per foot of applied pressure center column. These measurements were made from circumferential trenches with 2-inch PVC injection lines operated at flow rates of 0.15 to 0.22 gpm/ft. For injection lines without sheathed lines, α ranged from 0.01 to 0.46 gpm/lb. per foot of applied pressure.

The pressure required to deliver a given flow rate to a specified nozzles system may also be estimated from values for unit hydrostatic head by use of the following equation:

$$P_0 = \frac{Q}{2\pi k D_s L} \ln \frac{R}{L_c} \quad (4-3)$$

where P_0 is the applied pressure head, R is the effective well radius, and L is the range of influence. The radius of influence may be thought of as the distance beneath a horizontal line source at which the effect of the source becomes negligible.

Using these relationships, a system curve may be constructed from which a pump can be selected. The system "curve" for steady state injection into a well of length L , may be determined with the following equations:

$$P_0 + H = \frac{V_p^2}{2g} + \frac{fQ}{D} \frac{V_p^2}{2g} + (2k_s) \frac{V_p^2}{2g} + \frac{Q}{L} \quad (4-4)$$

$$P_0 + H = \frac{V_p^2}{2g} + \frac{fQ}{D} \frac{V_p^2}{2g} + (2k_s) \frac{V_p^2}{2g} + \frac{Q}{2\pi k_s D_s L} \ln \left(\frac{R}{L_c} \right) \quad (4-5)$$

where V_p is the pipe velocity, Q is the injected flow rate, f is the friction factor, D is the internal pipe diameter, and k_s is the sum of the solid flow coefficients.

Solid Matrix Properties

The hydrostatic compressibility of the undrilled solid matrix must be estimated to design the injection well system. The

hydraulic conductivity of soil has been reported in a number of studies, and the values have been found to vary greatly. A summary of reported soil hydraulic conductivities is presented in Table 4-1 and includes information regarding the vertical hydraulic conductivity determined at the RODS as a portion of study (Fauschett et al., 1990a). Also included in Table 4-1 are the estimated $|K_h|^{1/2}$ values resulting from the horizontal injection experiment at ACME (Chapter 3).

Since hydraulic conductivity values are the greatest unknown in this process, the pumping system should be designed to allow flexible control over the injected pressures and flow rates over an expected range of conditions. No benefit is homogeneous and this uncertainty requires that some degree of operational control be available after the system is in place.

Leachate collection system

Typical design of a leachate collection system often includes performing simulations with a hydrologic model to determine an infiltration rate for leachate into the concrete collection system drainage layer. From this, the flow into the DSI may be determined as a function of the characteristics of the DSI using a number of equations (Hoover 1989, Susong 1990). In the design of an RODS, the equations developed for the shape of the saturated flow zone may be employed to estimate the infiltration of leachate into the DSI. This allows the effect of continuous injection at large pressures to be predicted.

Table 4-1. Solid Matrix Hydraulic Conductivity

| Author(s) | Comment | Hydraulic Conductivity (m/day) |
|---------------------------------|--|---|
| Peng and Gosselink (1979) | Laboratory Tests, Strained Matrix | $1.8 \times 10^{-5} - 1.0 \times 10^{-4}$ |
| Korplak et al. (1984) | Laboratory Tests | $0.1 \times 10^{-5} - 1.0 \times 10^{-5}$ |
| Schutte et al. (1985) | Laboratory Tests | 1.4×10^{-5} |
| Schutte et al. (1989) | Leachate Test | $1.0 \times 10^{-5} - 1.3 \times 10^{-5}$ |
| Morimoto (1989) | SEEP Model Predicted Values | 2×10^{-5} |
| Townsend et al. (1990) | Leachate Test, Infiltration Tests ACCOL K_s | $3 \times 10^{-5} - 4 \times 10^{-5}$ |
| Shank (1991) | Leachate Test ACCOL K_s | $4.7 \times 10^{-5} - 4 \times 10^{-4}$ |
| This Study (Chapter 3) | Estimate from ACCOL ACCOL K_s | $2.3 \times 10^{-5} - 2.3 \times 10^{-4}$ |

*Based on $K_s/K_s = 100$

At an infinite distance beneath a horizontal injection well, the downward infiltration will equal the injected flow, or q_{inj} . The closer the DCS is located to the injection well, the greater the infiltration rate of tracer per unit area into the leachate collection system. Thus flow (q_{inj}) or infiltration rate into the DCS, may be determined for the entire width of the saturated zone using the following equation and Fig. 4(a) to determine α_{inj} :

$$q_{inj} = \frac{2E_{inj}}{Z_{inj}} \frac{L}{X_p} \quad (4)$$

In the design of a DCS, simulations should be performed which predict infiltration head above the liner resulting from infiltration at times when the depth of water is small. The various conditions developed in the injectable system should then be tested to determine if the three design requirements are met.

Conclusion

A method was utilized to design a horizontal injection leachate recycle system. The design was based on the hydrology along and spacing of the injection lines to maximize the distribution of leachate while minimizing potential flow surface coverage. The procedure involved the use of steady-state saturated flow experiments to approximate the spread of the saturated zone surrounding an injection line,

The production of Isobutene generation rates and relative movement rates requires the use of more sophisticated numerical models, which account for the many complexities of a landfill.

ADDITIONAL FEATURES may assist the design and operation of a 3D-CFD. The method outlined here should generate guidelines for 3D-CFD design, and which should allow flexibility to examine various scenarios to meet specific goals in 3D-CFD design. Additional work in the application of this technology to other sites will aid in the determination of the effects of the many additional factors that will ultimately require consideration.

CHAPTER 8 TERMINAL AND CONSOLIDATION

This chapter will review the use of a technology known as horizontal injection leachate recycle. This technology enables leachate which has been treated in the solid waste of a landfill to still be reintroduced to the landfill waste. The advantages of leachate recycle are many, and include the following.

1. Leachate recycle provides a means of hydrologic management at landfill sites.
2. The reapplication of leachate promotes the acceleration of biological stabilization of the solid waste.
3. Recycled leachate removes some treatment from the biologically active landfill.
4. A landfill which has been biologically stabilized presents a substantially reduced risk to the environment as a source of landfill leachate.
5. Biological stabilization may obviate the need for landfill closure and may allow the landfill to be stabilized naturally.

Horizontal injection is one of several methods of leachate recycle, and the advantages of this method include:

1. Leachate may be recycled to the landfill without direct exposure to the atmosphere.
2. The power of leachate application may be controlled, allowing the flexibility to target specific areas and

levels within the landfill, as well as the rate and frequency of application.

b. Horizontal injection will have little impact on daily landfill operations as regard to surface area requirements and the movement of landfill vehicles and equipment.

c. Horizontal injection will allow the addition of various chemical or biological additives to the landfill.

The major limitation for the application of horizontal injection at full-scale landfills is the lack of full-scale operational experience to provide the design, construction, and operations guidelines. This study was designed to provide such information.

A method of analyzing the predicted rates of saturated flow resulting from the injection of liquids into a porous medium was developed by treating the injection line as a line source. To facilitate the solution in the form of simple analytical equations, capillary forces and dispersion were neglected. The resulting solution was useful for the predicting flow boundaries for certain flow conditions which must be used in design, but are not intended to model liquid wastes transport in complex systems. Equations were developed for isotropic and anisotropic media to determine the steady state zone of saturation surrounding an injection well resulting from injection at a given flow rate.

This study assessed the construction and operations of a RI-LIS at a municipal landfill operating landfill in Florida. Construction of injection lines at the Florida landfill began

in 1993, and the first injection began in 1995. Through August 1994, a total of 7,000,000 gallons of leachate were infiltrated into 11 injection lines. The system was successful in providing a means of recycling large volumes of leachate to the landfill. The most dramatic problem associated with the operation of the RI-CAT was the short-circuiting of leachate to the surface through permeable areas in the landfill. Typical leachate flow rates ranged from 0.004 to 0.007 gallons per foot of applied load at a flow range of 1.0 to 3.0 gpm/ft. In general, flow did decrease over time in a stabilized subset.

This document outlines guidelines for the design, construction, and operation of RI-CAT at solid-waste landfills. The information gathered in the field research project and the theoretical flow equations were used to outline a preliminary design technique and procedure. The technique was developed to allow estimates for the spacing of injection lines, placement and operation of lines to preclude the seepage of leachate to the surface, and the placement and operation of lines for the design of leachate collection systems. The procedures outlined are proposed as a method for the design and operation of a RI-CAT which in turn will allow additional field data to be gathered for the refinement of the design of such systems.

The operation and design of infiltrated leachate recycle systems were reviewed in regard to the specificities of the landfill environment and the potential for infiltration.

design of the landfill components like piping and pump sizing, DO₂ oxygen - addition areas that influence the design of an injection system may include:

1. The effect of leachate application on biodegradability of the landfill microorganisms.
 2. The hydrology of the entire landfill area.
 3. Use of the site to collect landfill gas.
 4. The effect of leachate recycle on leachate quality.
- Additional field studies at the sites discussed here and other sites be mandatory for further development of this system.

APPENDIX A LEACHATE INJECTION GRAPHS

This appendix presents graphs of the data collected for the horizontal injection line series at ASCEI. The results cover injection times 1 through 11, and were a period from February 1993 through August 1994. The following graphs are presented for each injection line:

- I. Injection flow and pressure versus calendar time (day 1 represents January 1, 1993).
- II. Injection flow and pressure versus pumping time.
- III. Linear flow rate and total energy head vs. residence of injection line versus pumping time.
- IV. Linear flow potential energy head ratio (ψ) versus pumping time.

Key to the data in graphs of pumping time and cumulative pumped volume requirements: injection times where data loggers were lost. Total volume and pumping time were accounted for in these cases.

Legend: The following graphs were formatted so flow is reported by the thicker solid line and pressure by the thinner dotted line. The flow is generally scaled higher than the pressure.

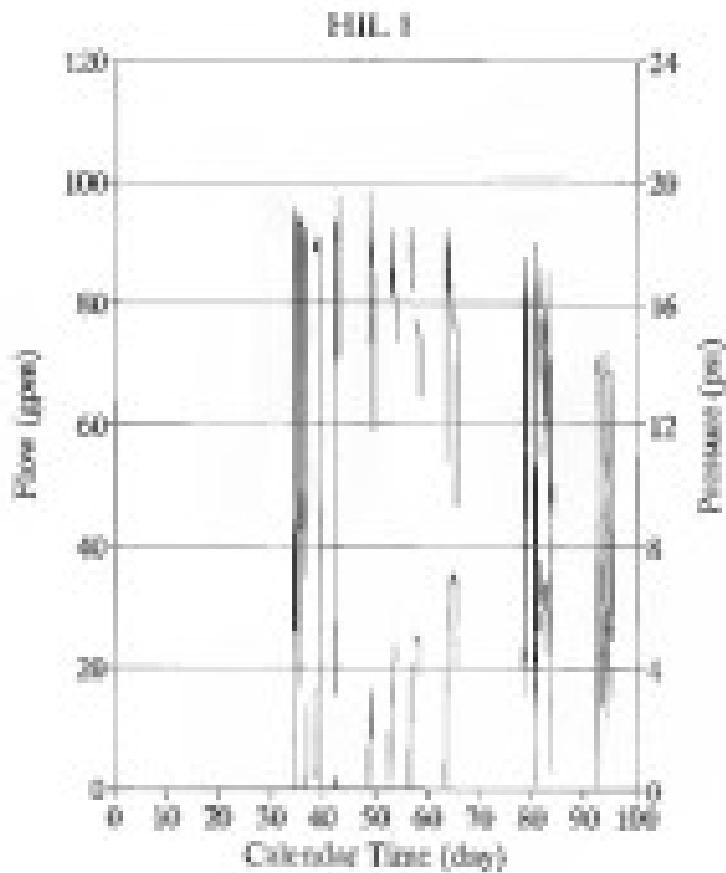


Figure 4-3. Injection Flow Rate and Pressure versus Calendar Time: HIL 1 (February 1993 - April 1993).

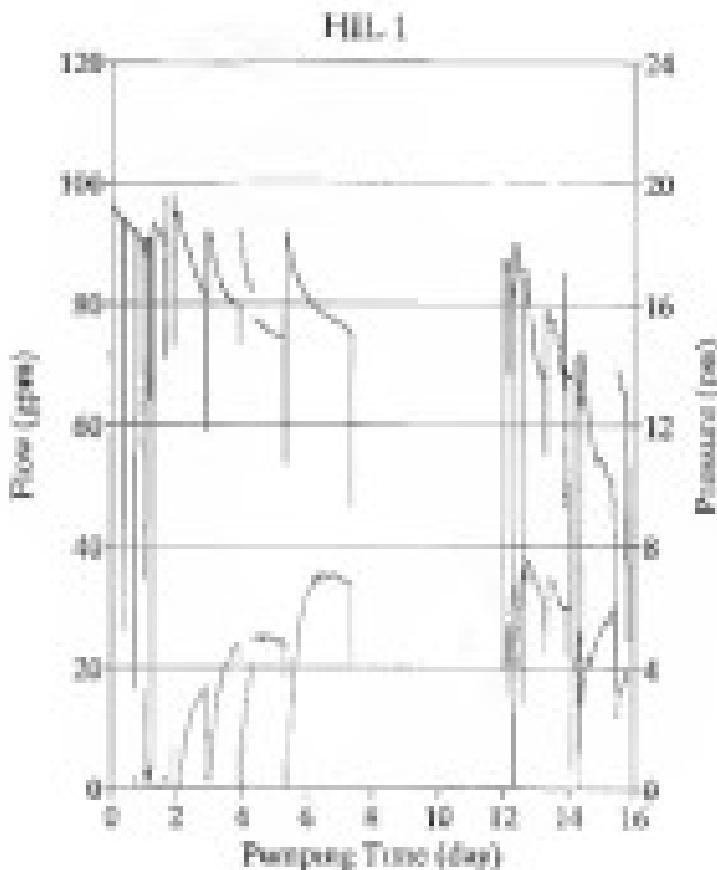


Figure 2-2. Injection, Pump Rate, and Pressure versus Pumping Time from HIL 1 (February 1992 - April 1993).

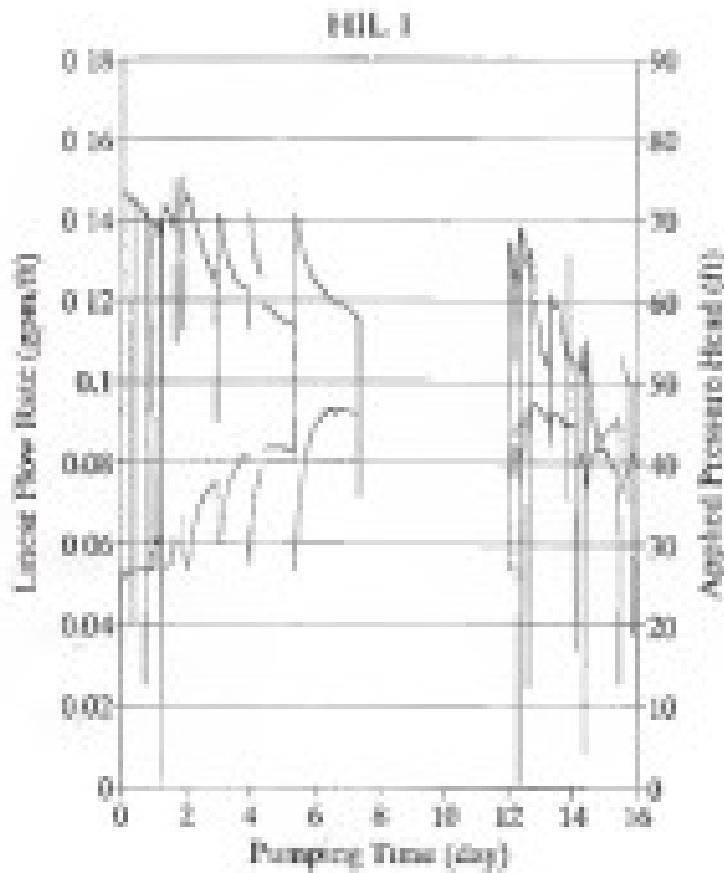


Figure A-3. Linear Flow Rate and total Applied Head versus
28) Pumping Time, HIL 1, (February 1979 - April 1980)

HL. 1

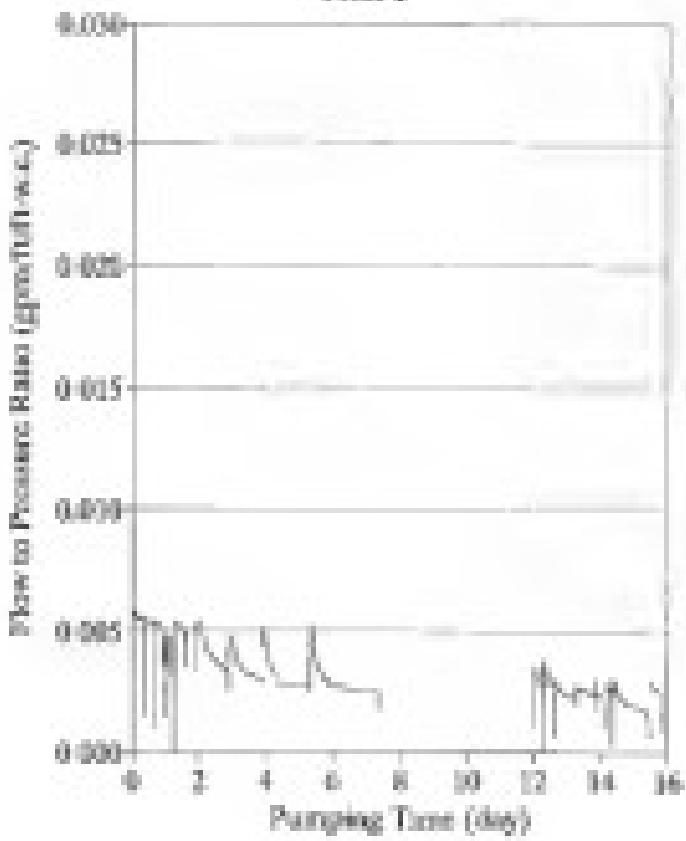


Figure 4-4. A versus Injection Time HL. 1
(February 1992 - April 11 1992)

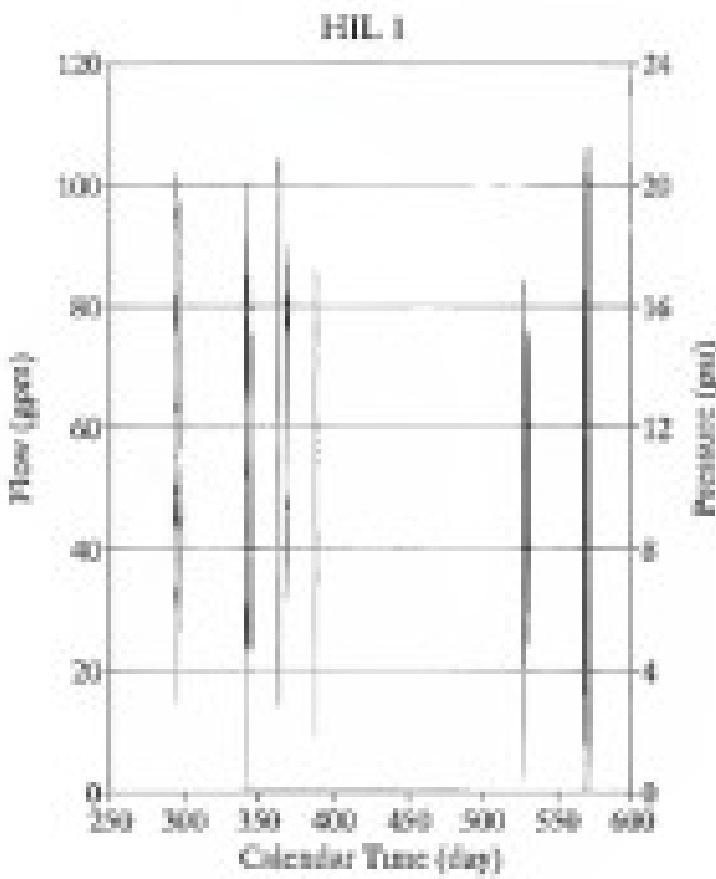


Figure A-2. Injection Flow Rate and Pressure versus Calendar Time: HIL 1 (September 1993 - August 1994).

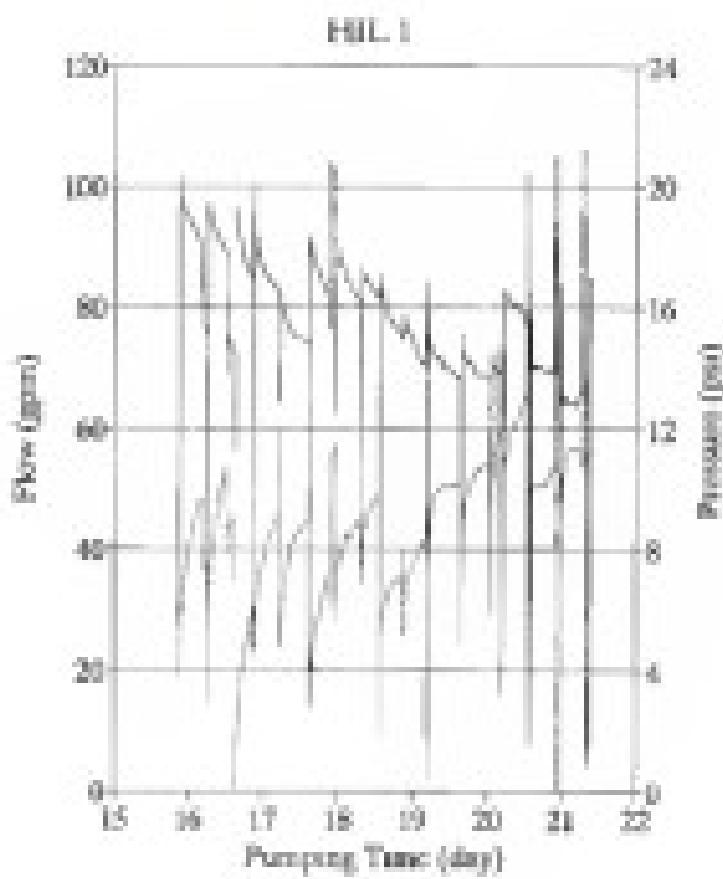


Figure 4-6. Injections Flow Rate and Pressure versus Injections Time - HIL 1 (September 1993 - August 1994).

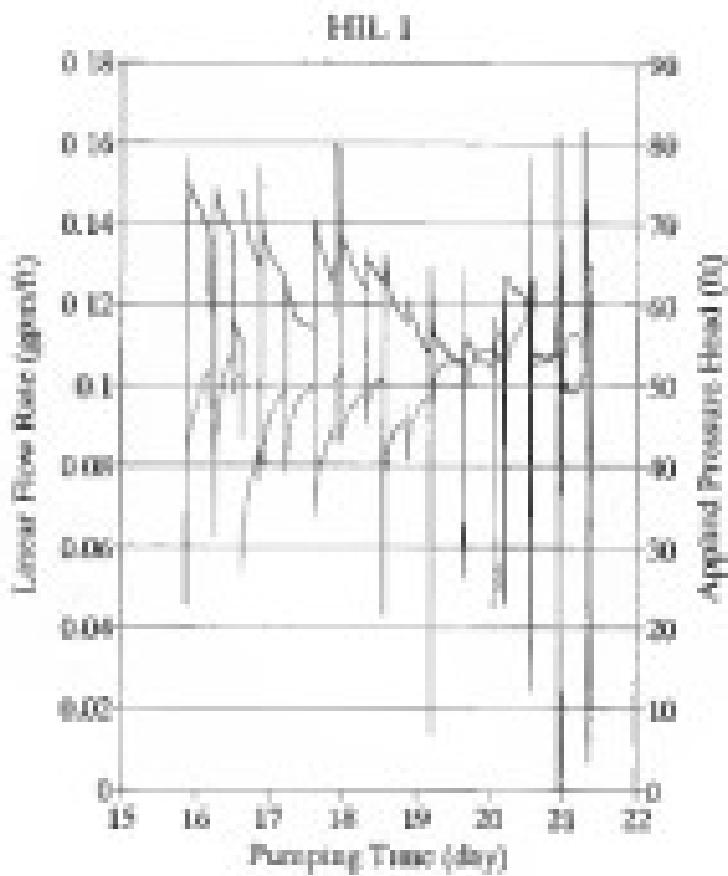


Figure 8-7. Linear Flow Rate and Total Applied Head versus
Pumping Time: HIL 1 (September 1983 - August 1984).

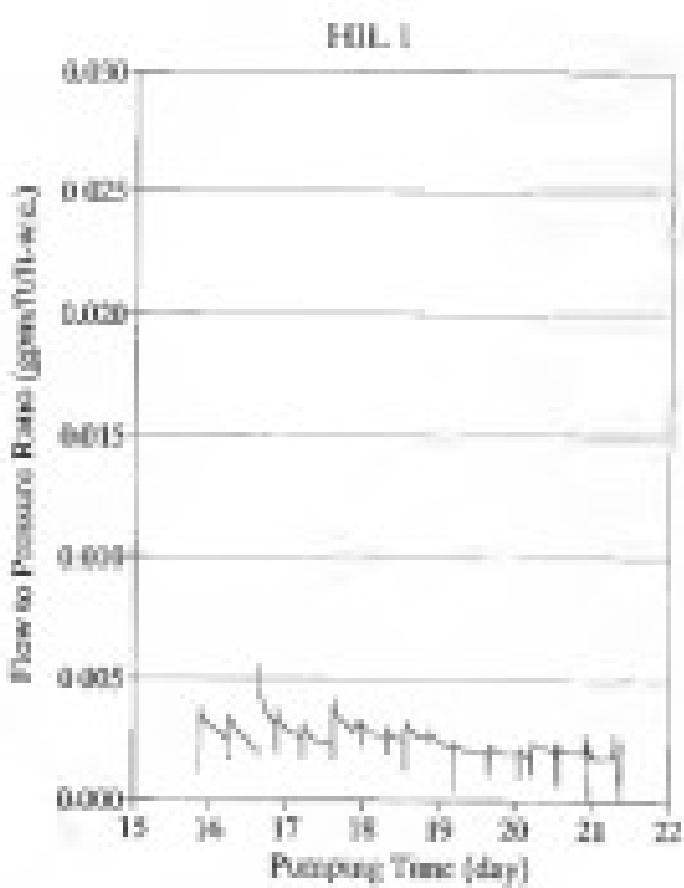


Figure 2-4. α versus injection time: HIL I
(September 1988 - August 1990)

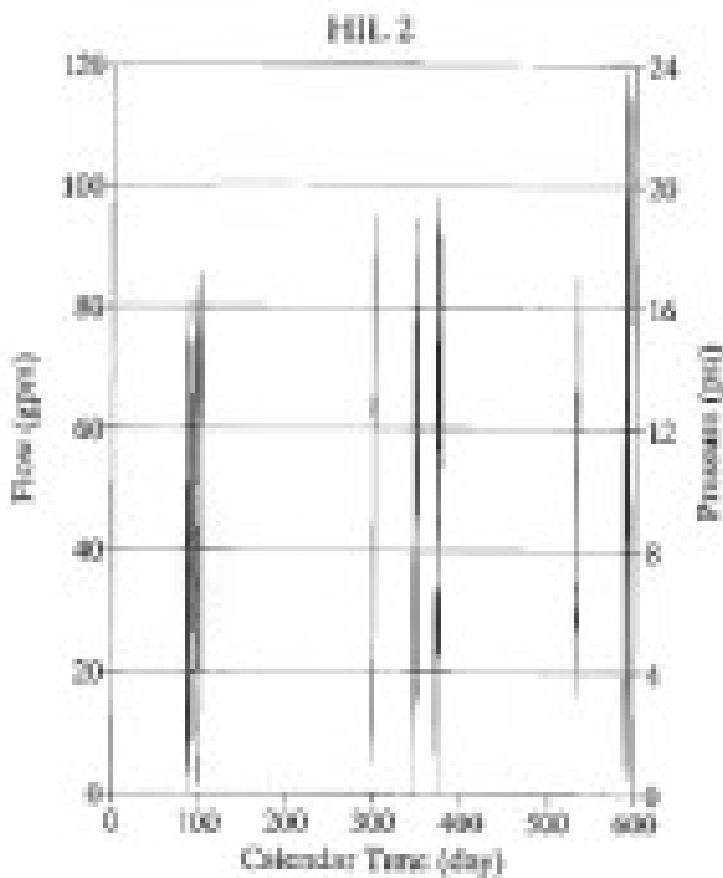


Figure 2-8. Defining Flow Rate and Pressure versus Calendar Time. HIL 2

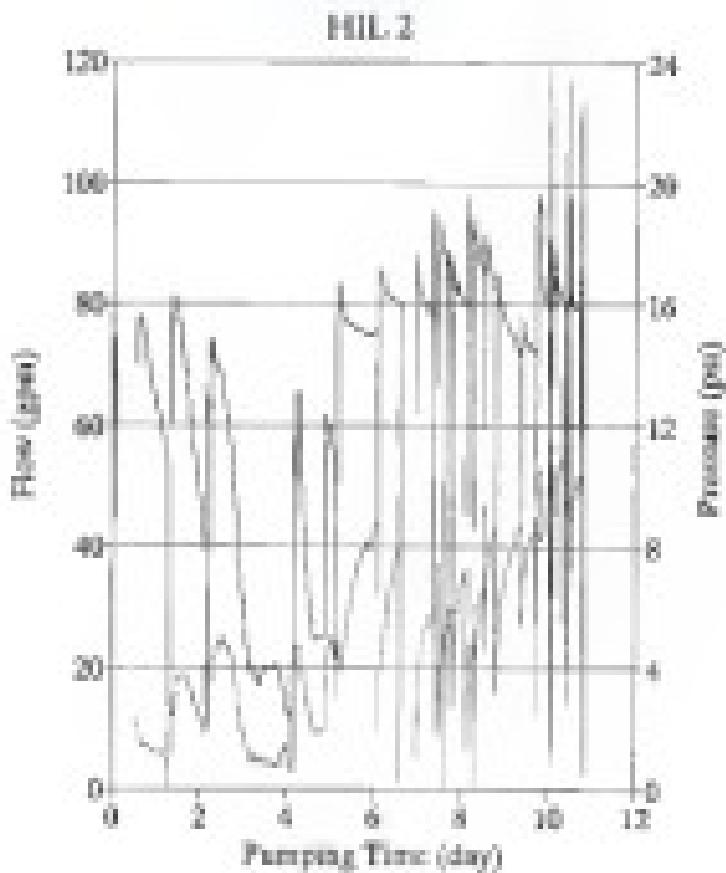


Figure 8-18. Injection Flow Rate and Pressure versus Injection Time - HIL 2.

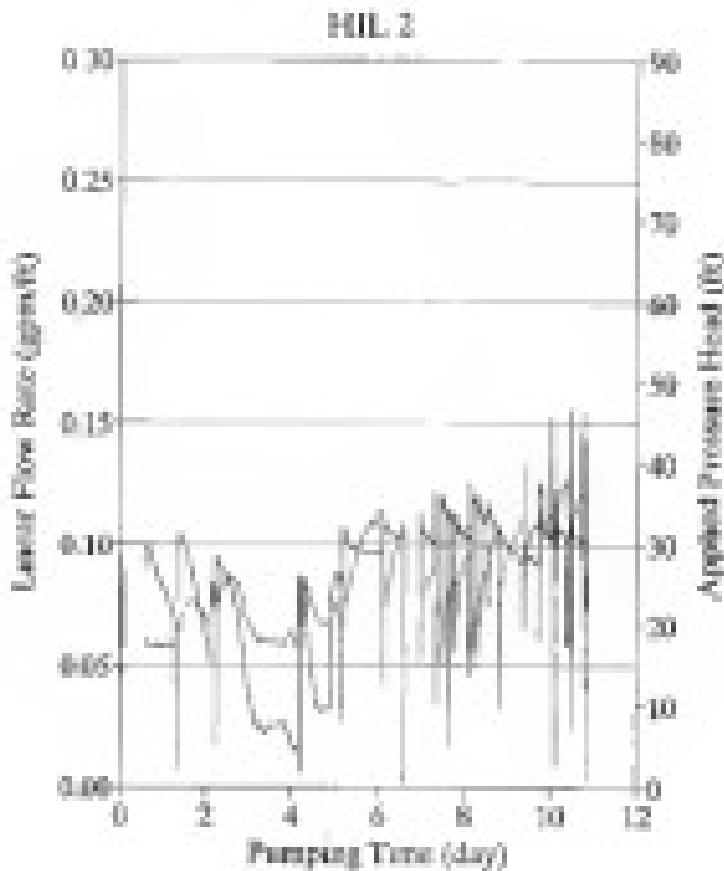


Figure 8-12. Litter flow rate and total applied head versus pumping time, HIL 2.

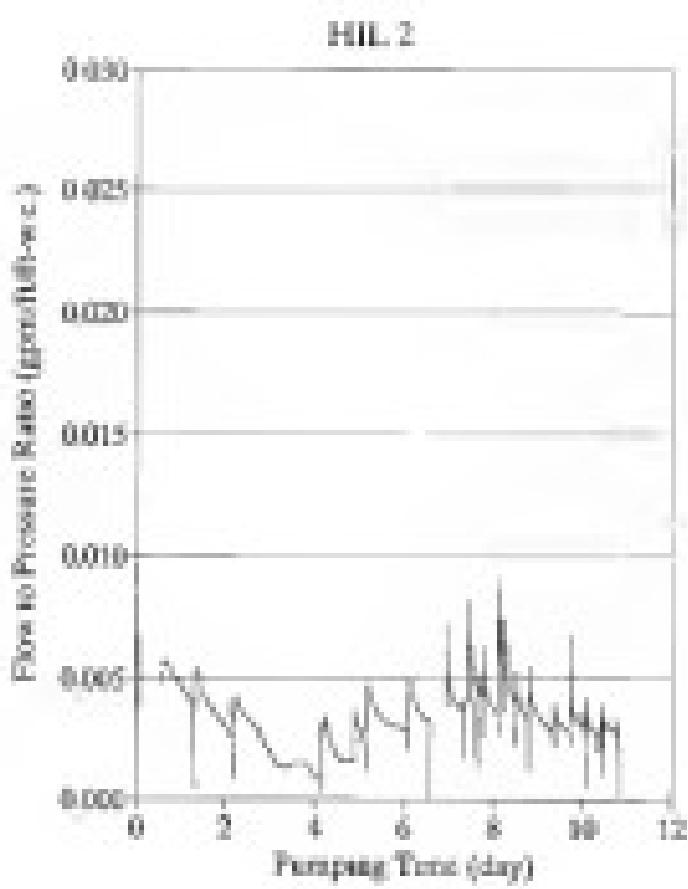


Figure A-13. η versus injection time; art. 3

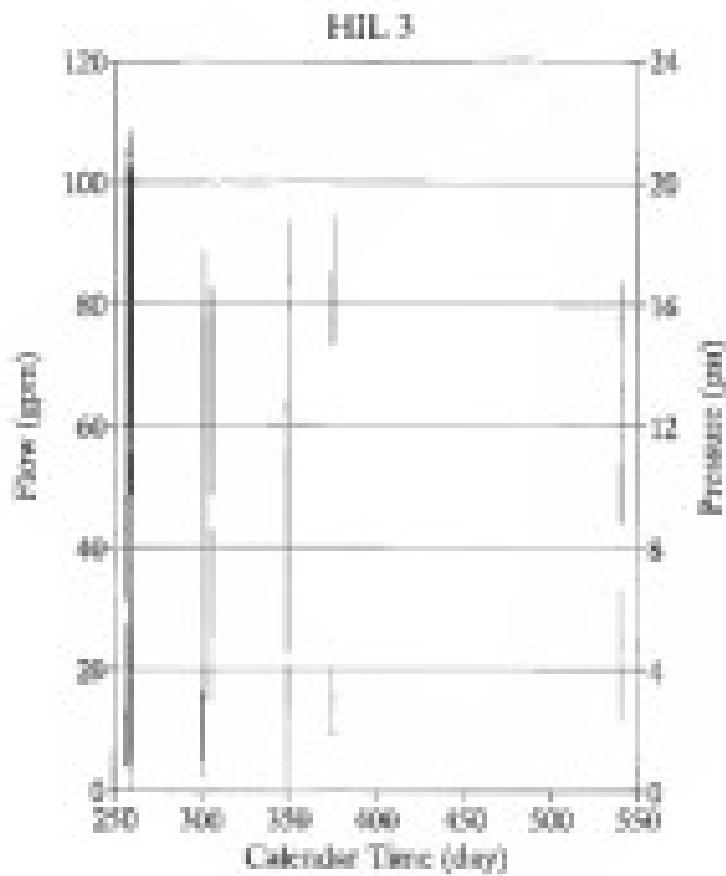


Figure 8-18. Injection Flow Rate and Pressure versus Calendar Time (HIL 3).

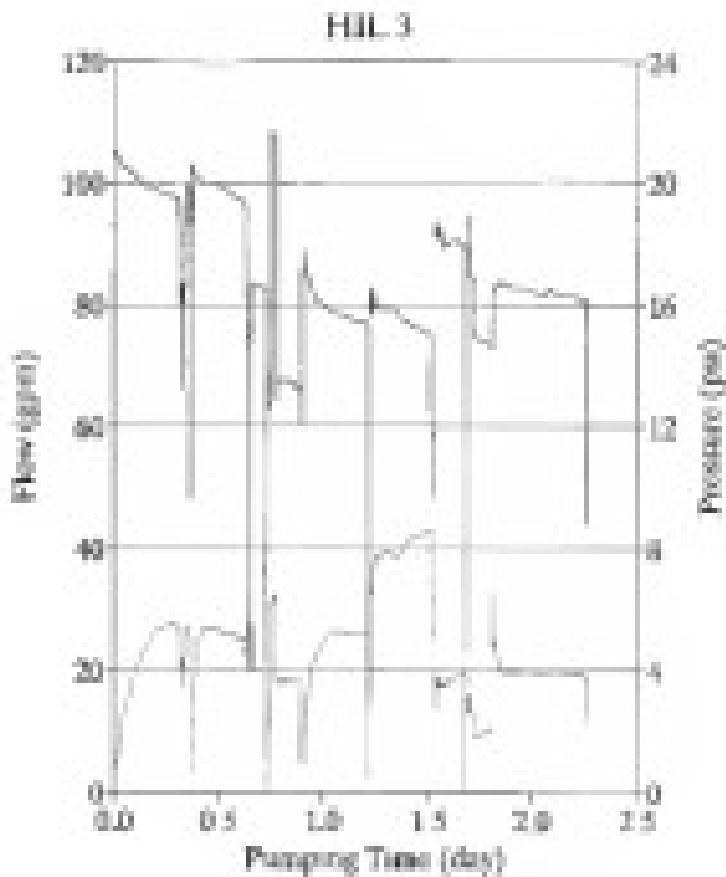


Figure 4-24. Injection Flow rate and Pressure versus
Injection Time, HIL 3

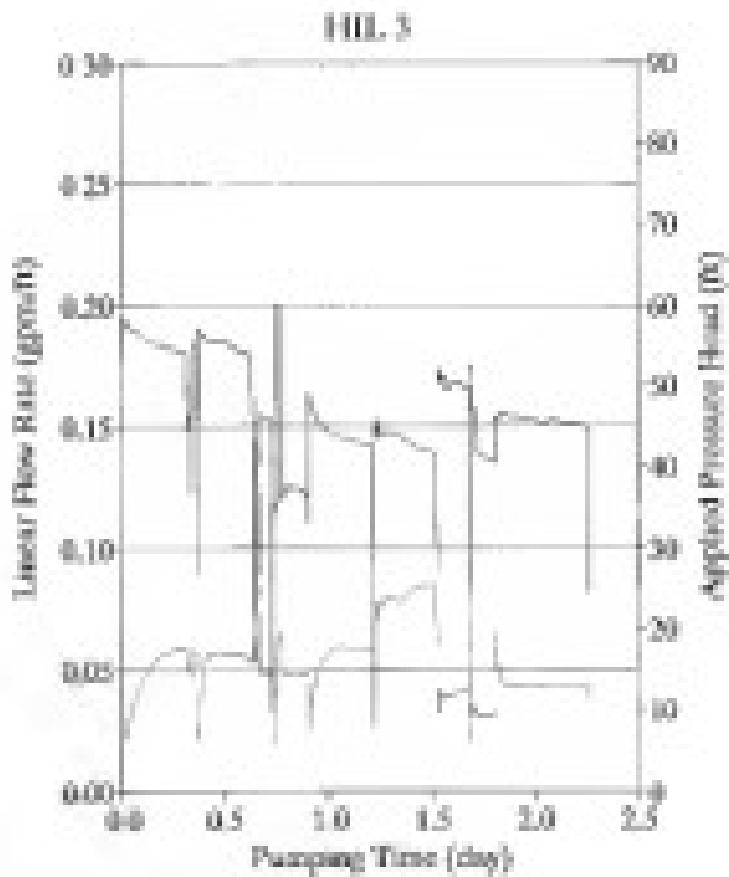


Figure 3-18. Linear flow rate and total applied head versus pumping time, HIL 3.

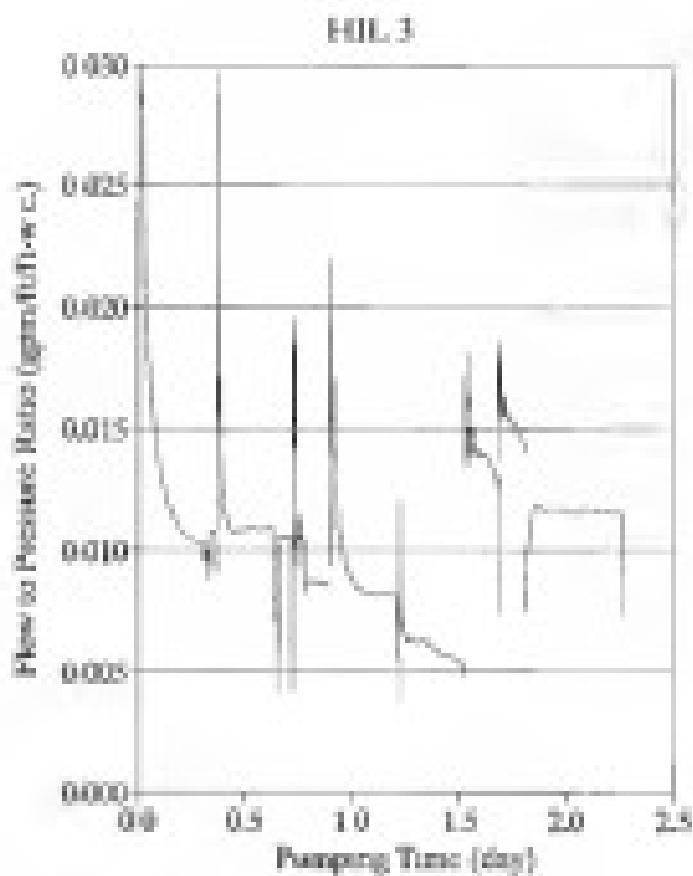


Figure 3-14. η versus Deposition Time: HIL 3

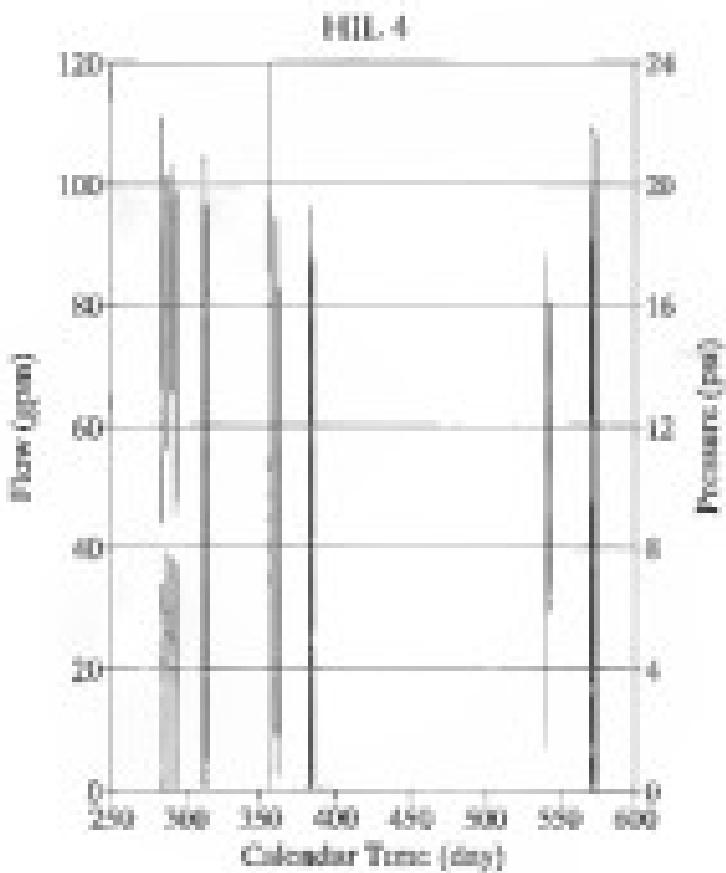


Figure 3-17. Injections: Flow Rates and Pressure versus Calendar Time, HIL-4

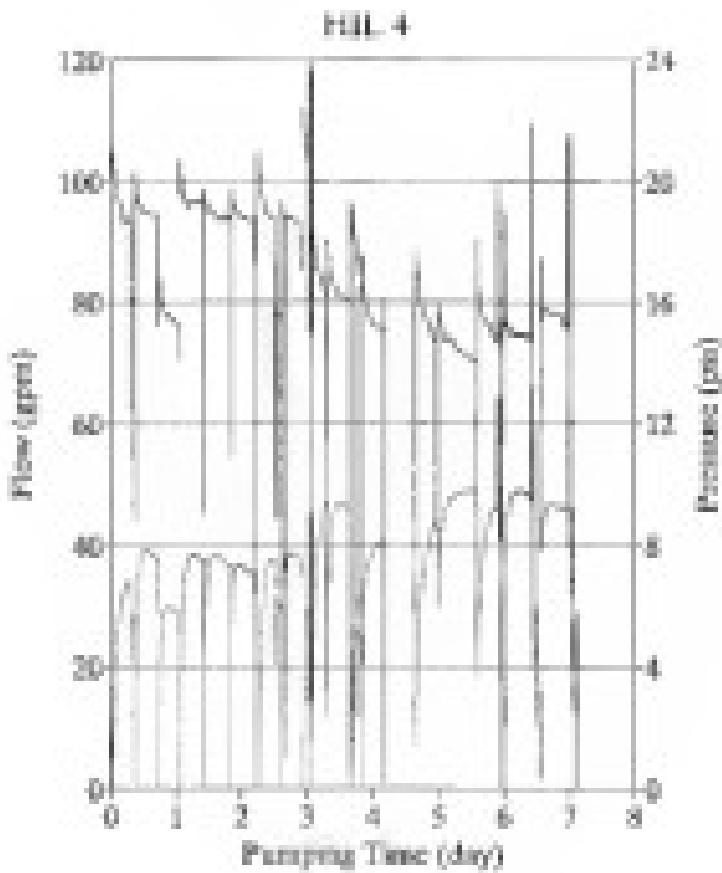


Figure 4-26. Injection Flow Rate and Pressure versus Pumping Time (HIL 4).

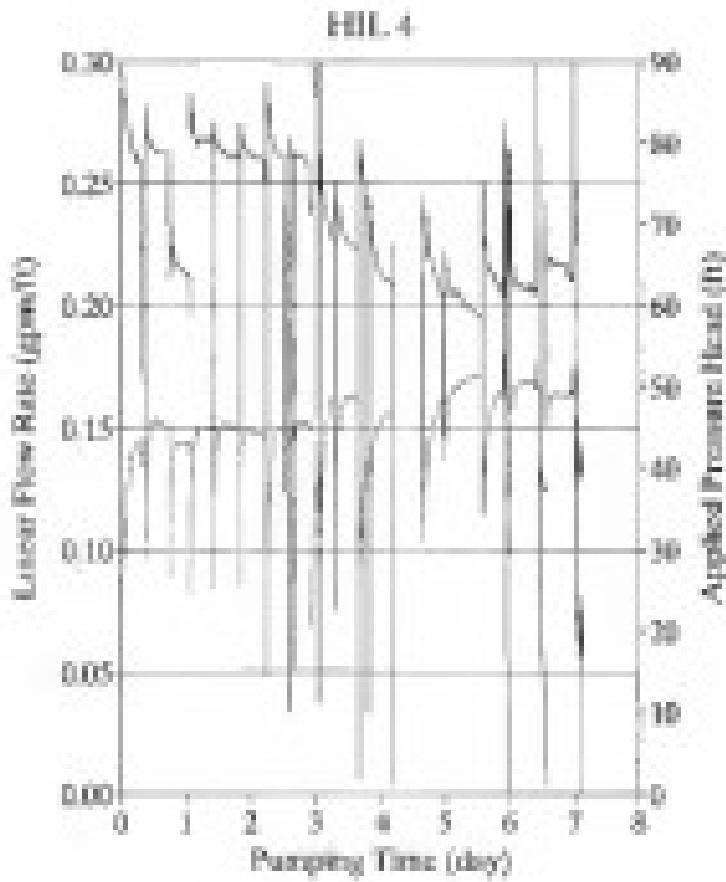


Figure A-18. Linear Flow Rate and Total Applied Head versus Pumping Time, HIL 4.

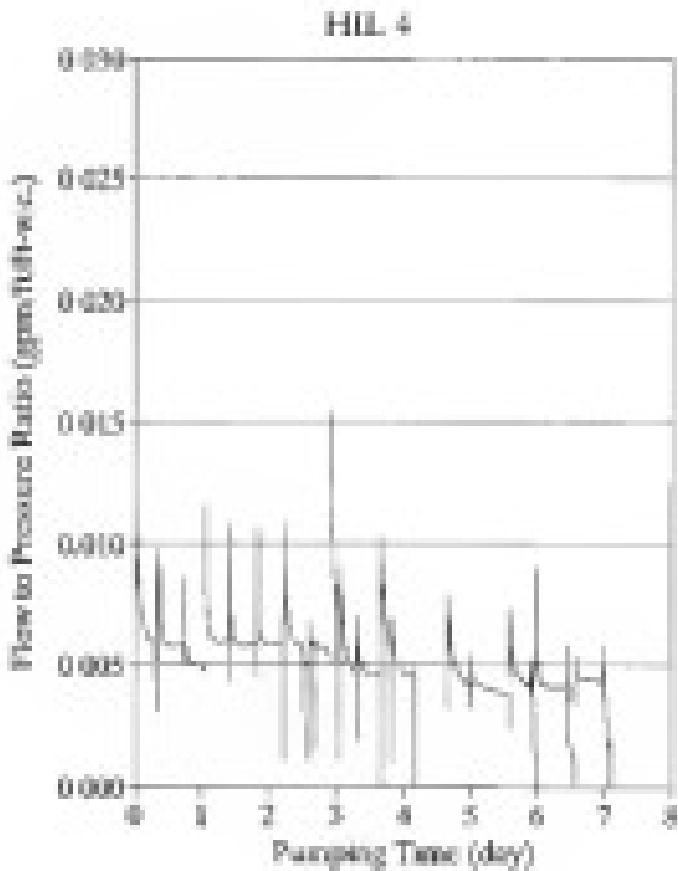


Figure A-20. A versus injection time: HL 4

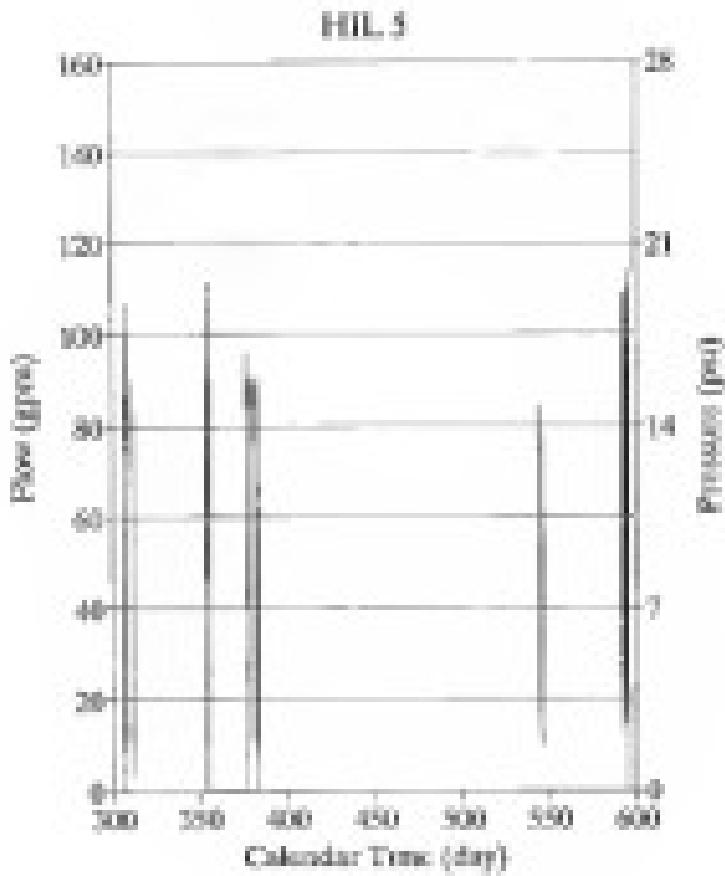
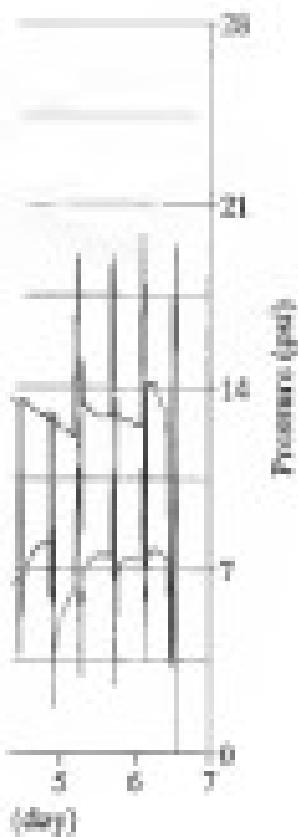


Figure 2-21. Injection flow rate and pressure versus calendar time. HIL 3.



Temperature and Pressure versus
Day. 5 = 0000 UTC 25 January 1990.

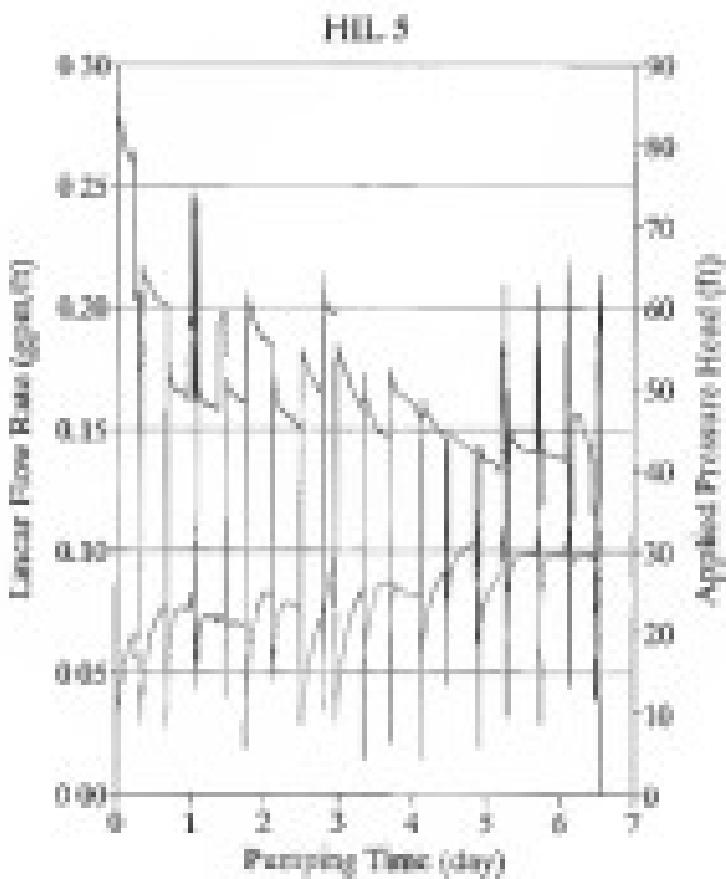


Figure A-28. Linear Flow Rate and Total Applied Head versus Injection Time, HIL 5.

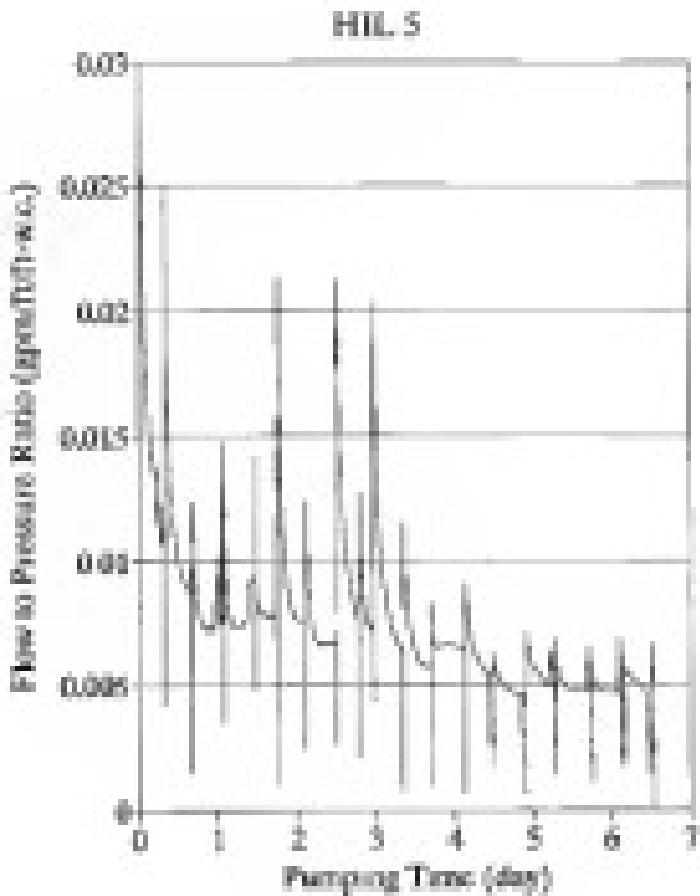


Figure 2-24. α versus Injection Time HIL 5

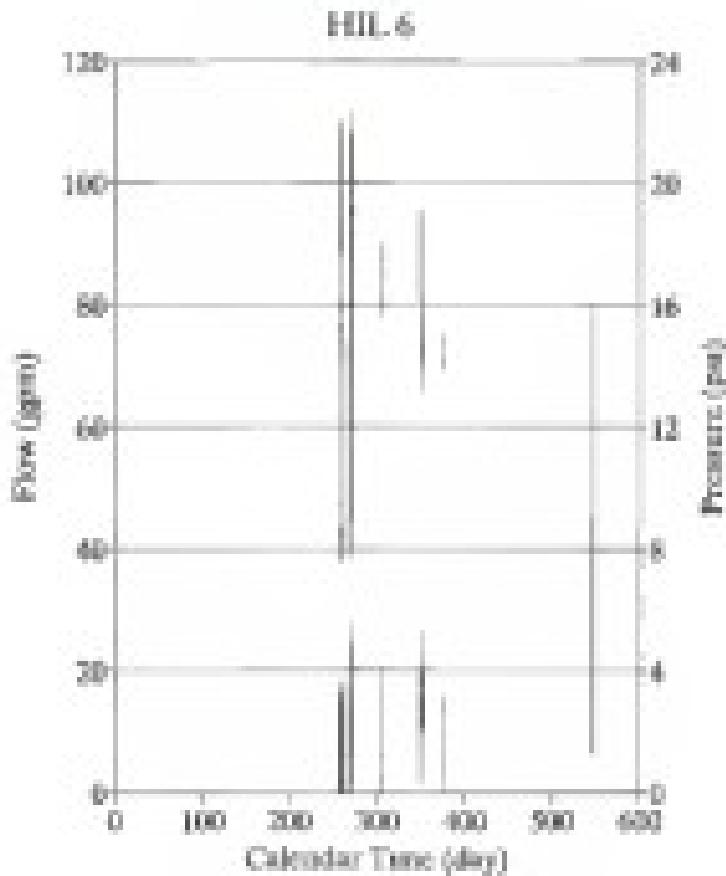


Figure 4-26. Ingestion Flow Rate and Pressure versus Calendar time, HIL 6.

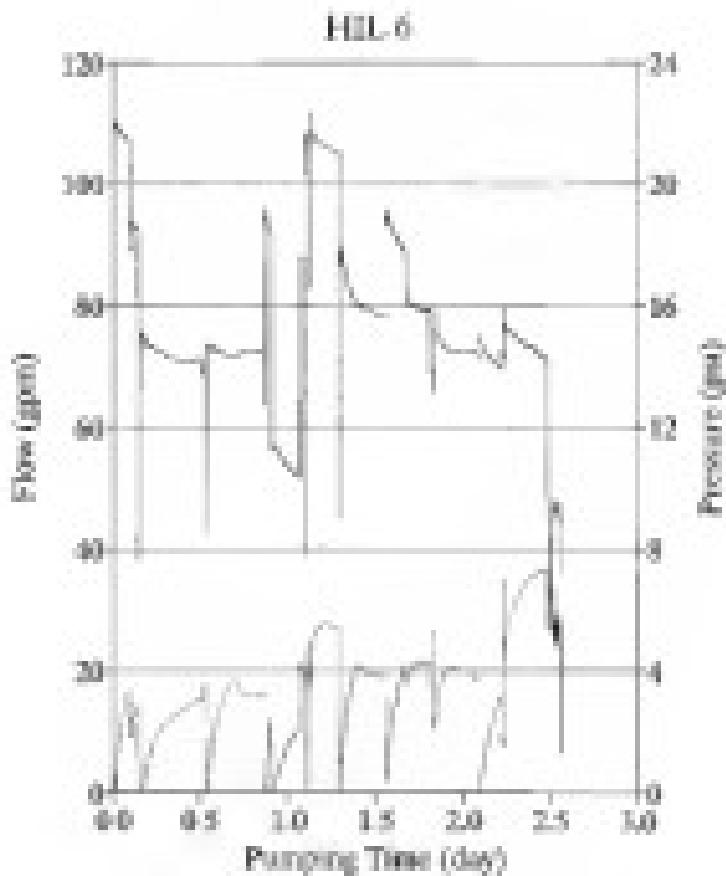


Figure A-10. Injection flow rate and pressure versus injection time. Well 6.

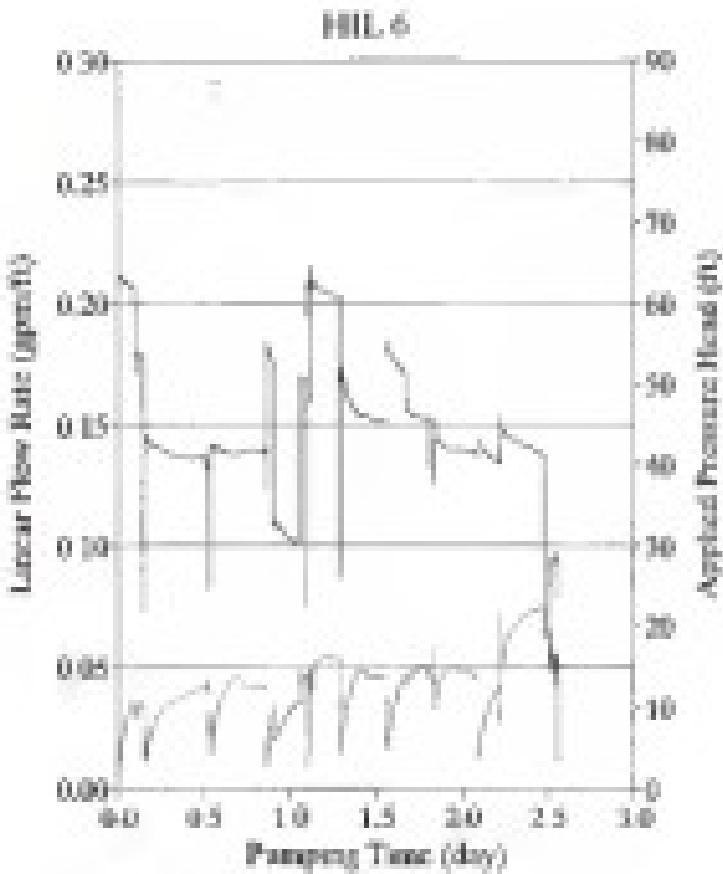


Figure 4e22. Linear Flow Rate and Total Applied Head versus injection time, HIL 6.

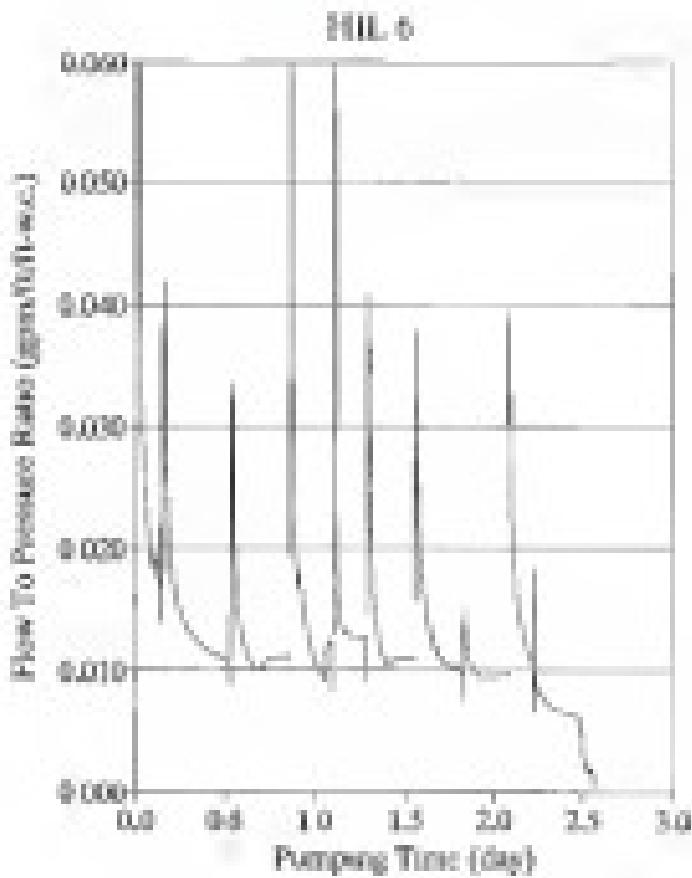


Figure 3-28. π versus Injection time, HIL-6

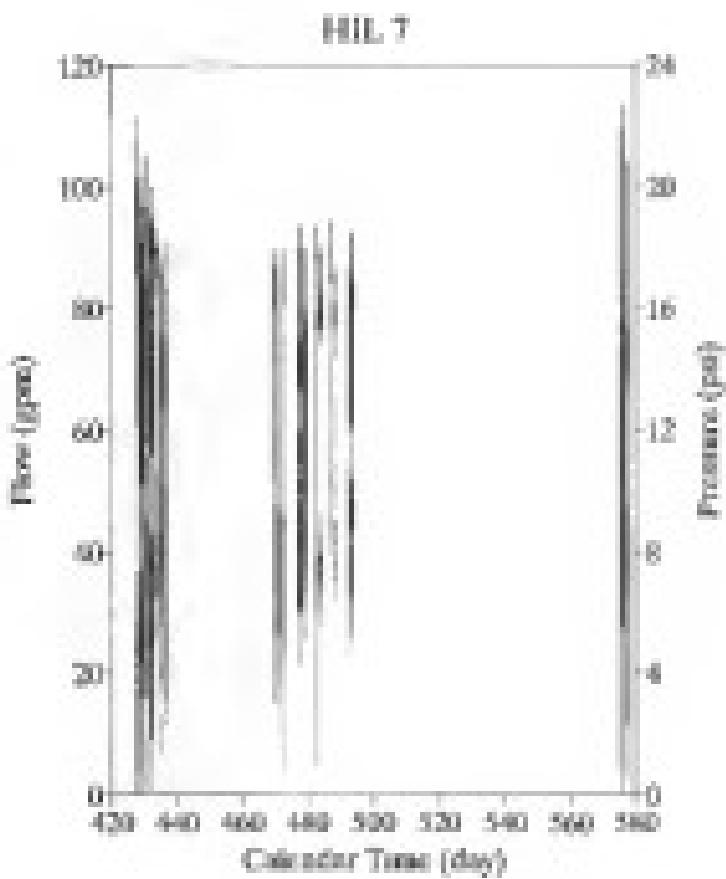


Figure A-21. Injection Flow Rate and Pressure versus Calendar Time; HIL 7.

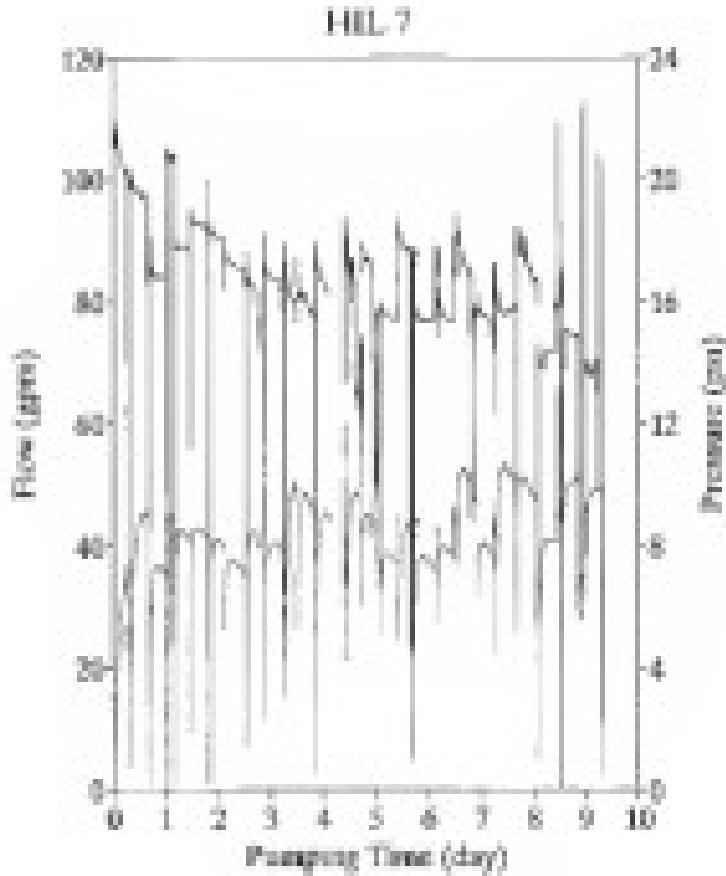


Figure A-29. Injection Flow Rate and Pressure versus Injection Time: HEL 7.

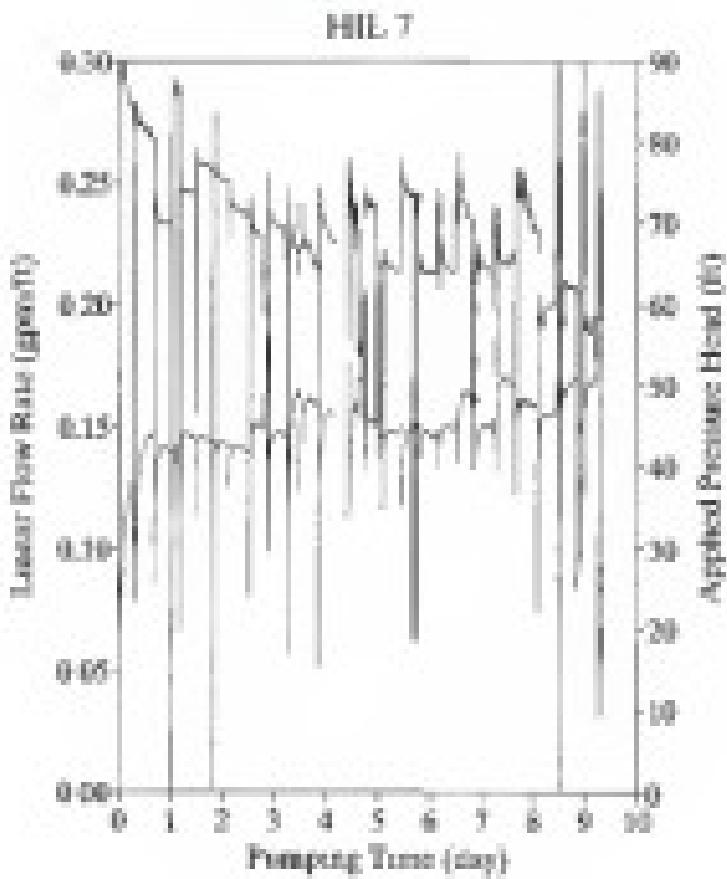


Figure 8-32. Linear Flow Rate and Total Applied Head versus
Injection Time: HIL 7

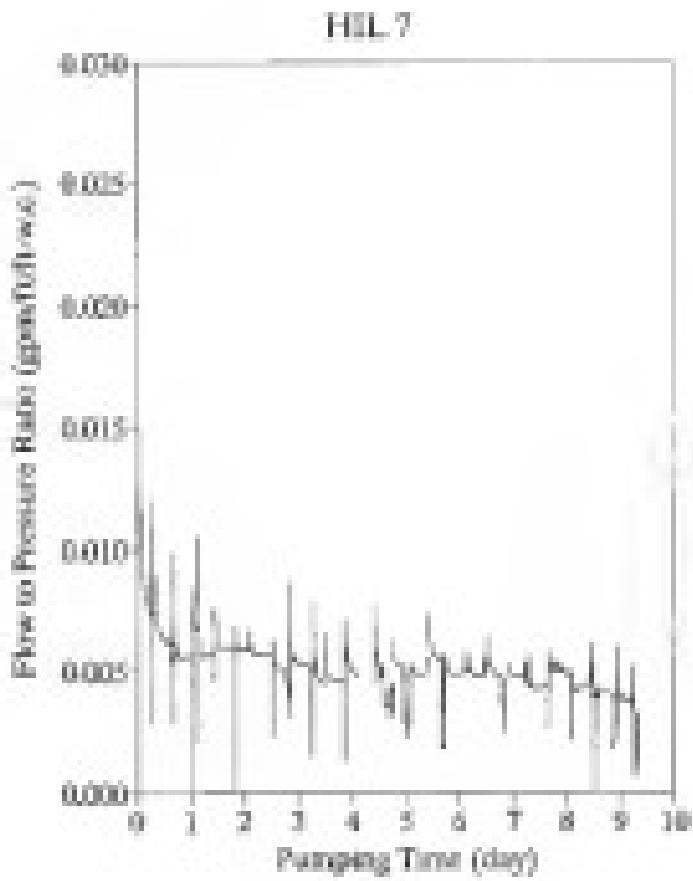


Figure 2-12. A normal injection flow HEL 7

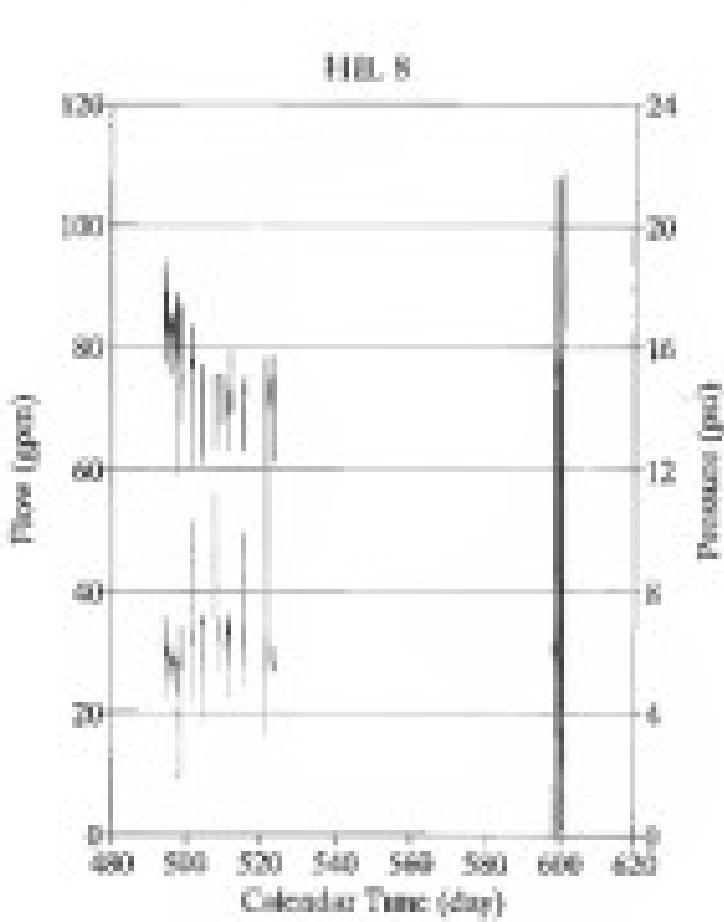


Figure A-2b. Injection Flow Rate and Pressure versus Calendar Time: HIL 8.

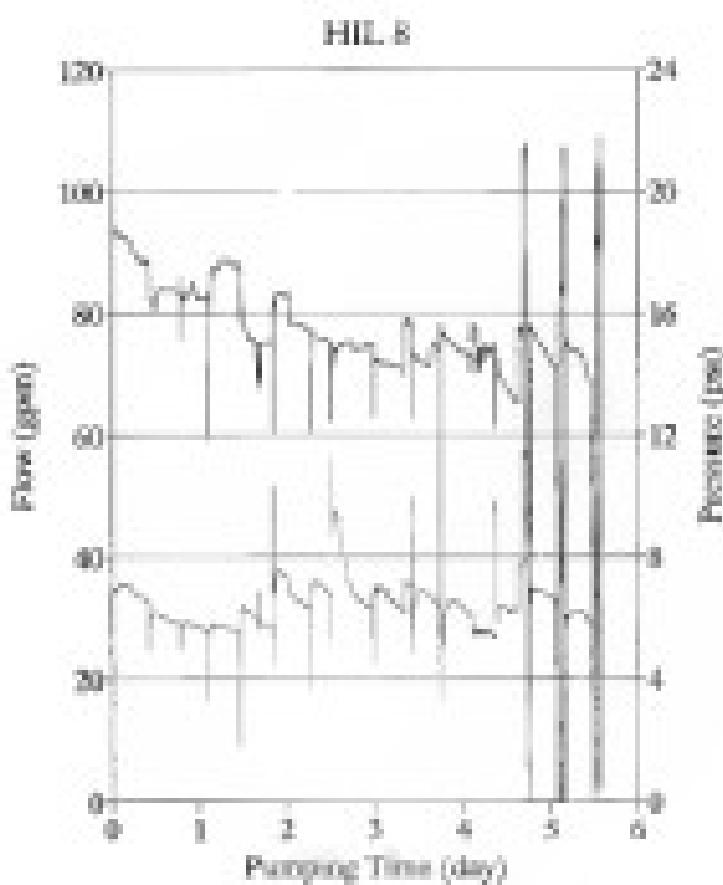


Figure 8-14: Injection Flow Rate and Pressure versus
Injection Time, HIL 8

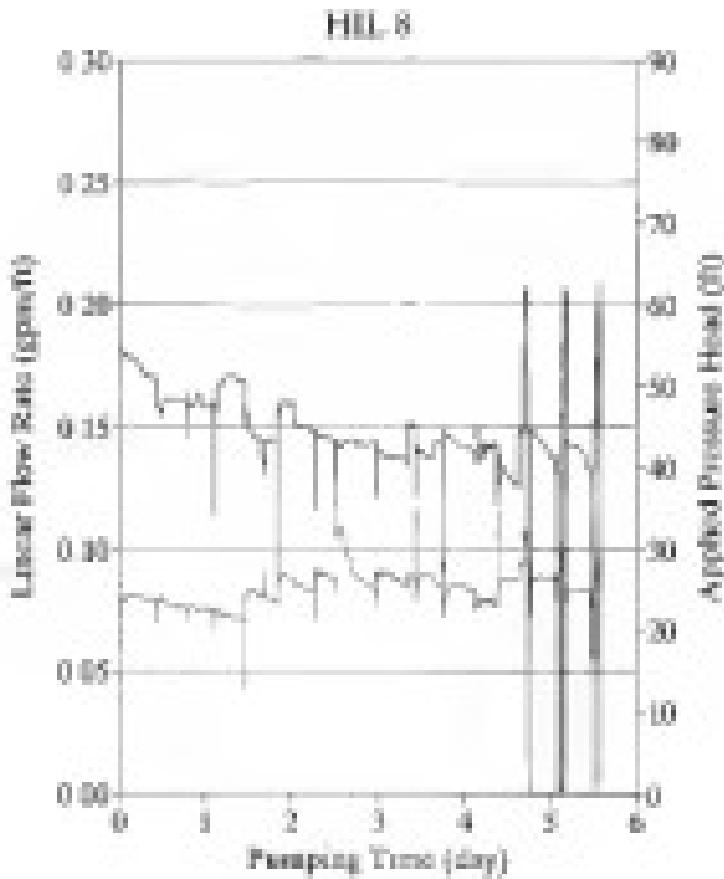


Figure A-34. Linner Flow Rate and total applied head versus pumping time HIL-8.

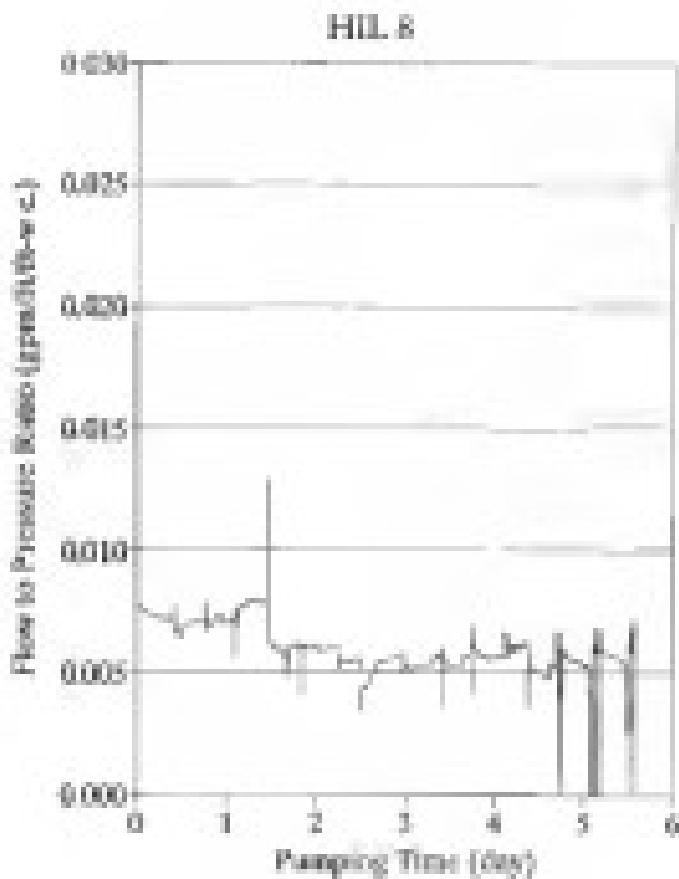


Figure A-38. a. Various Injection Times (HIL 8).

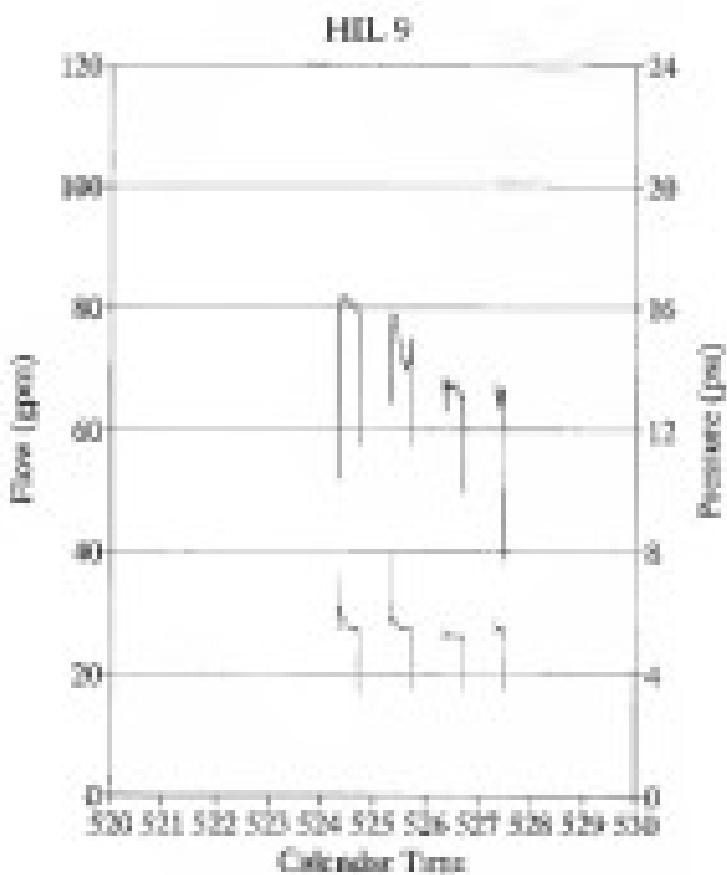


Figure A-97. Injection Flow Rate and Pressure versus Calendar Time: HIL 9

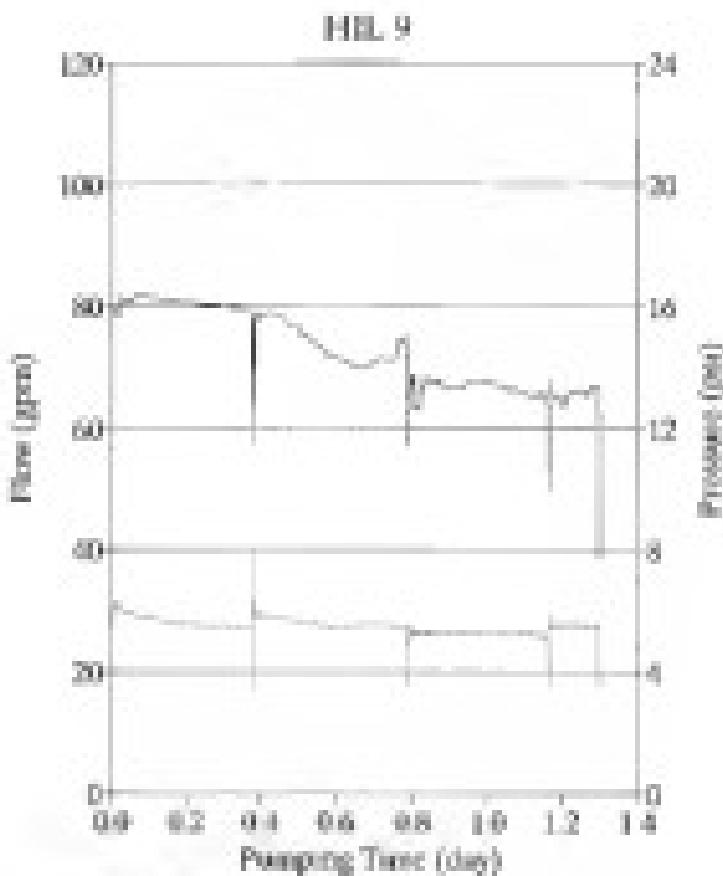


Figure 2-1a. Permeate Flow Rate and Pressure versus Pumping Time for HL 9.

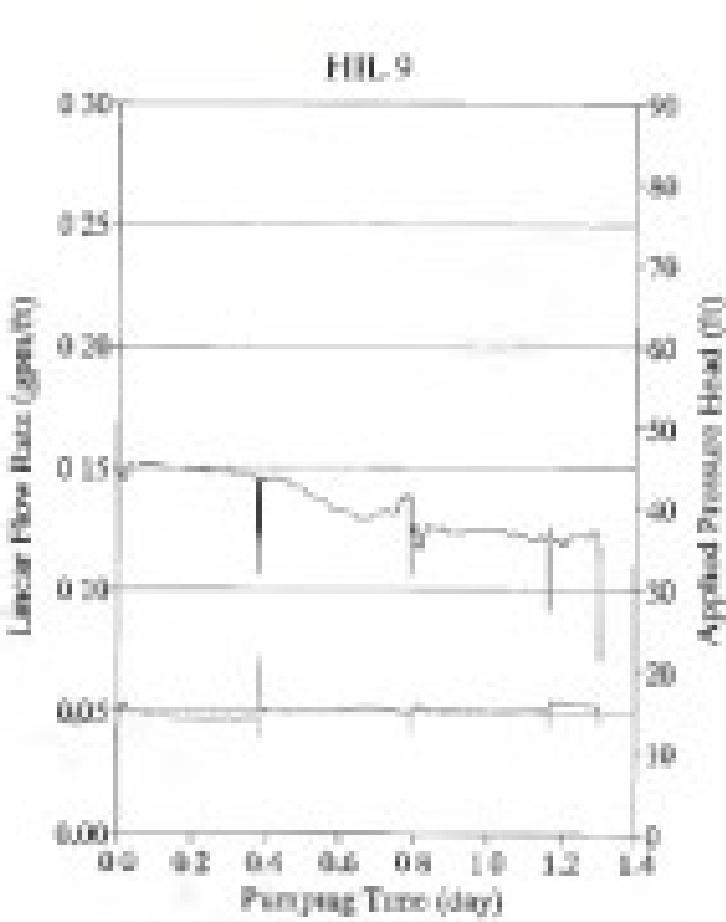


Figure A-29. Linear Flow Rate and Total Applied Head versus Deposition Time: HIL-9.

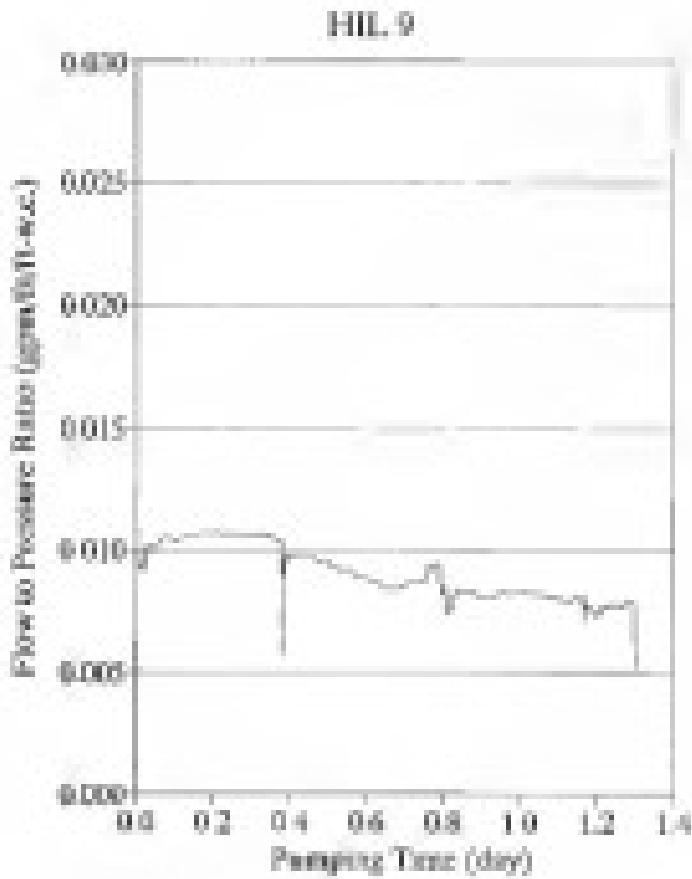


Figure 2-10. A Return Injection Time: HIL 9

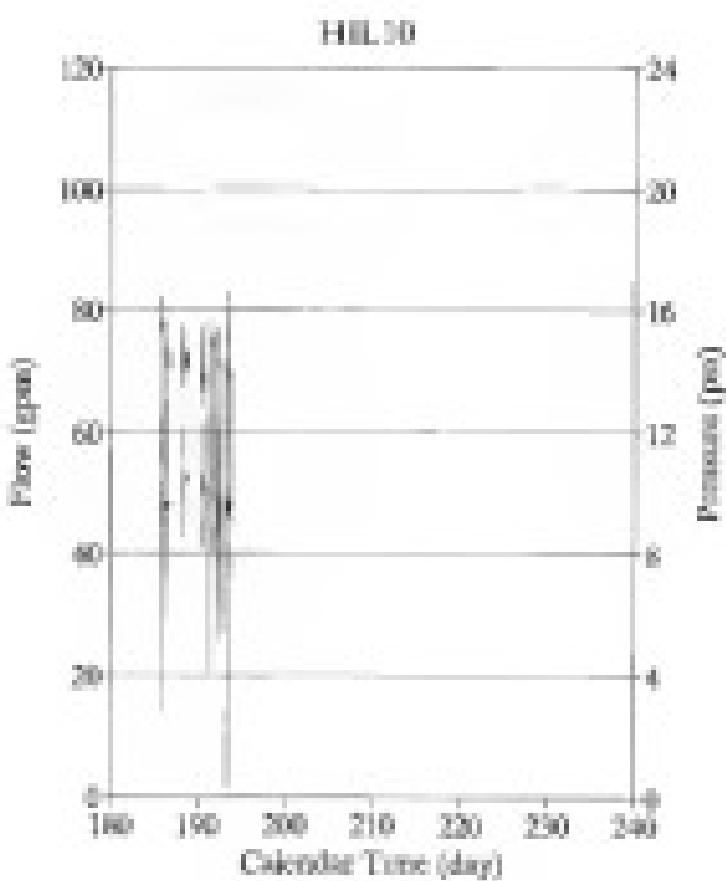


Figure A411. Inportion Flow Rate and Pressure versus Calendar Time: Run 10.

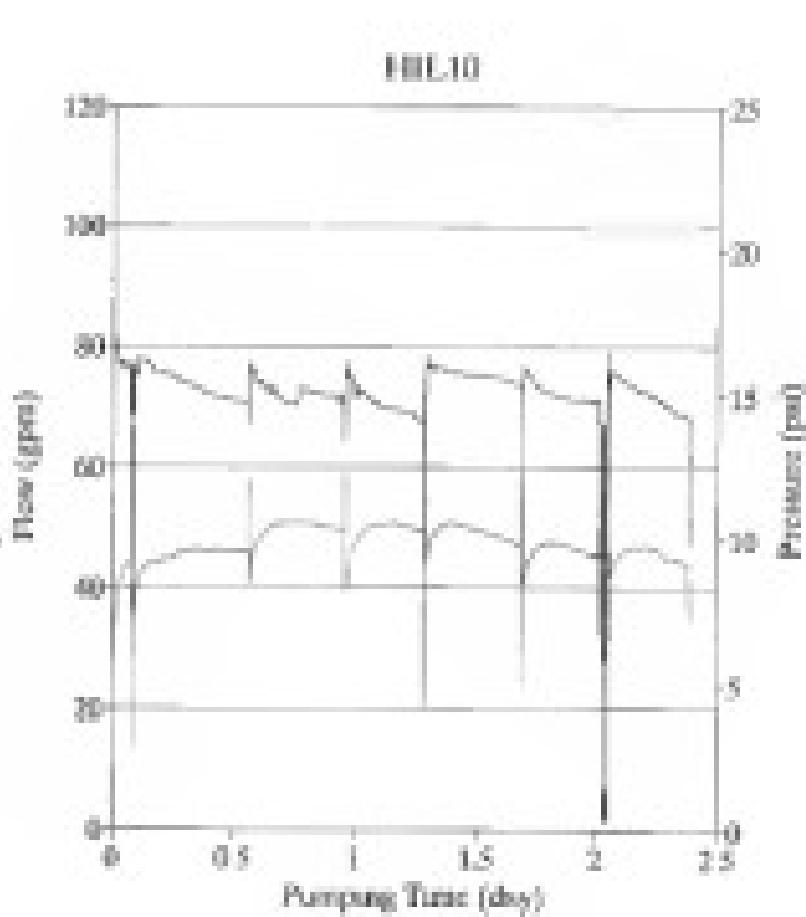


Figure A-61. Injection Flow Rate and Pressure versus Injection Time, Well 10.

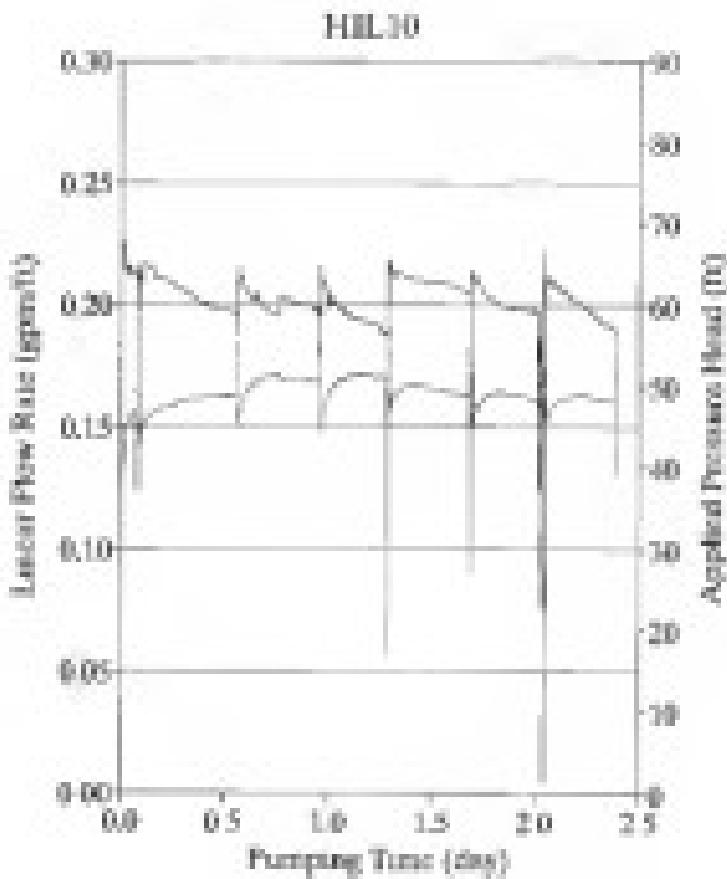


Figure 3-43. Linear Flow Rate and total Applied Head versus Pumping Time, HIL30.

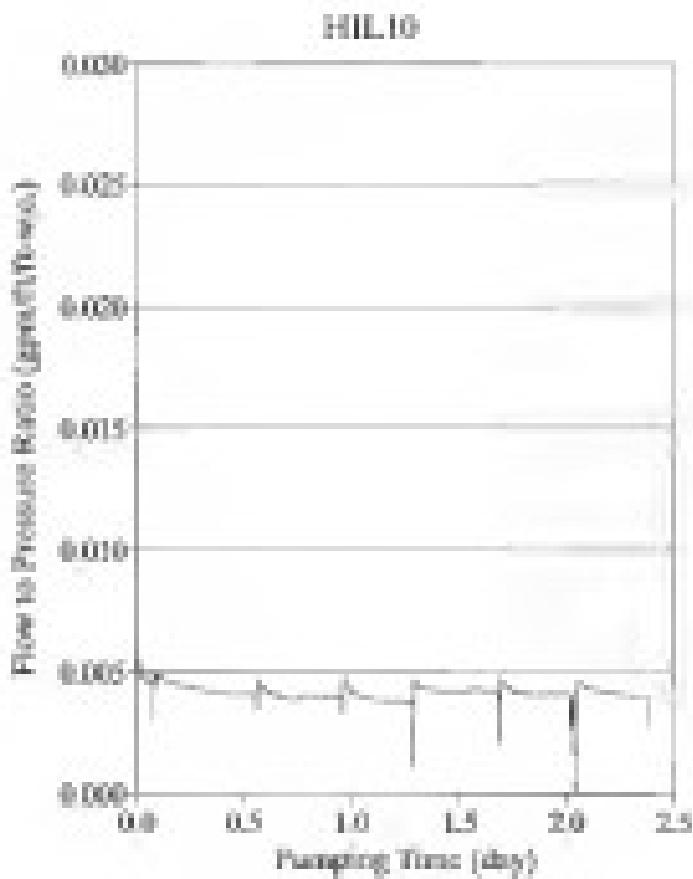


Figure A74A: 8. Various Injection Times: HIL 10

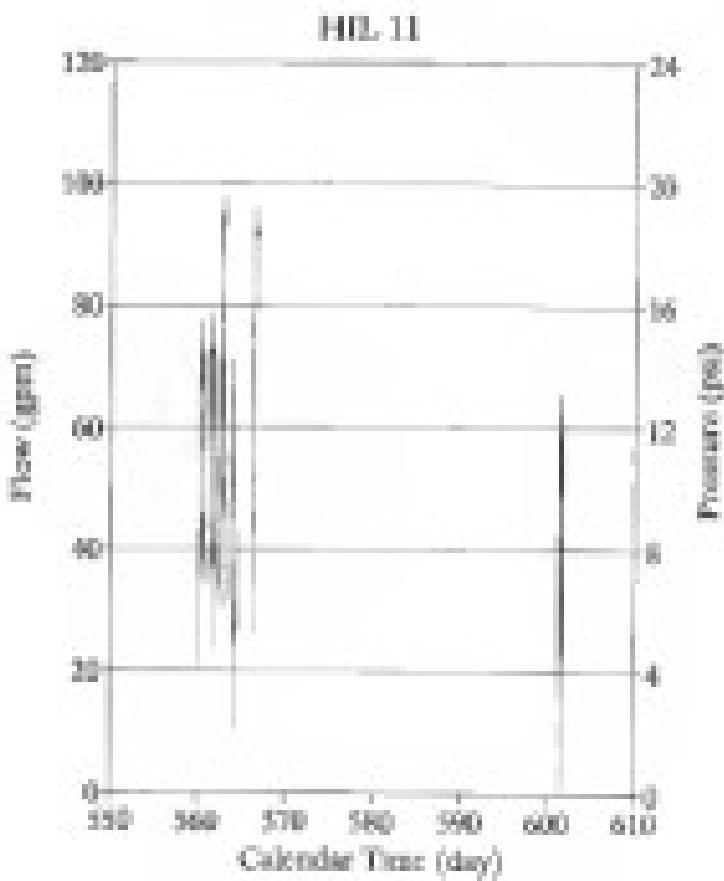


Figure 2-10. Injection Flow Rate and Pressure versus Calendar Time, KIL 10

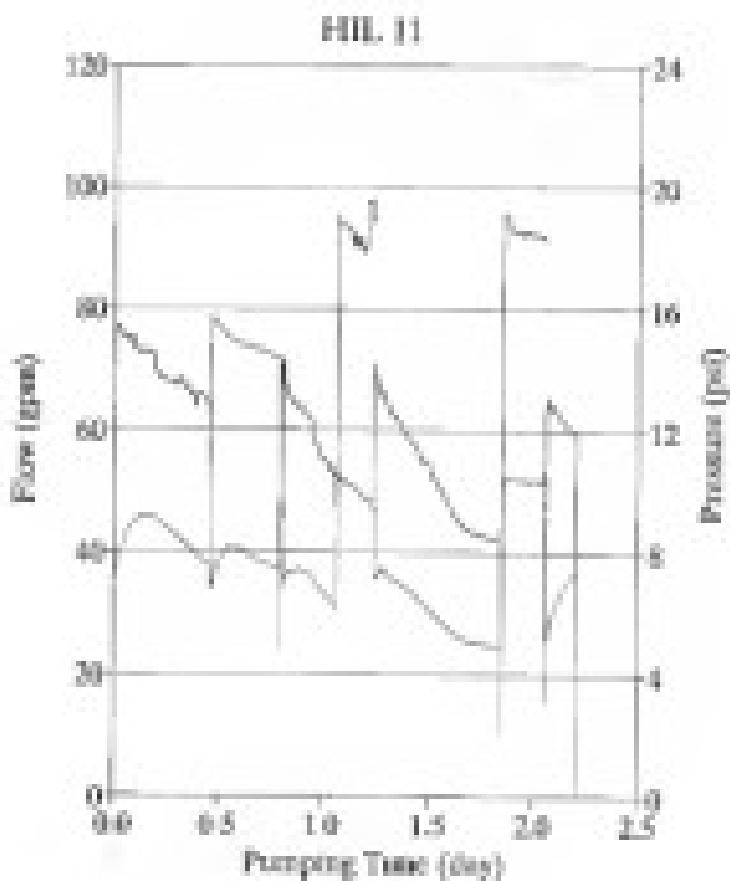


Figure 3-46. Injection Flow Rate and Pressure versus
Injection Time—HIL. II

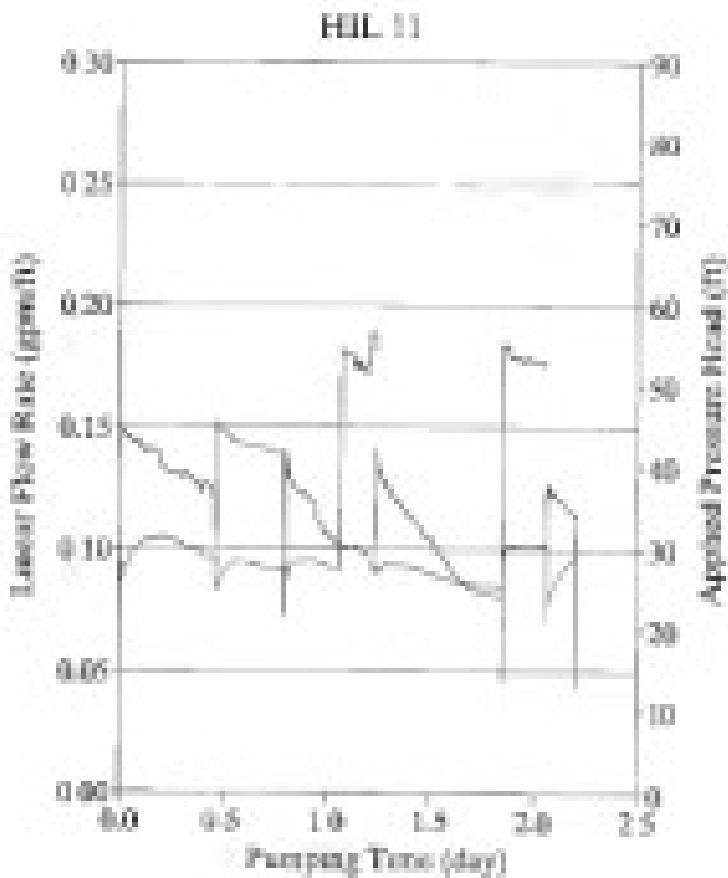


Figure 8-47. Linear Flow Rate and Total Applied Head versus Injection Time with 10 days.

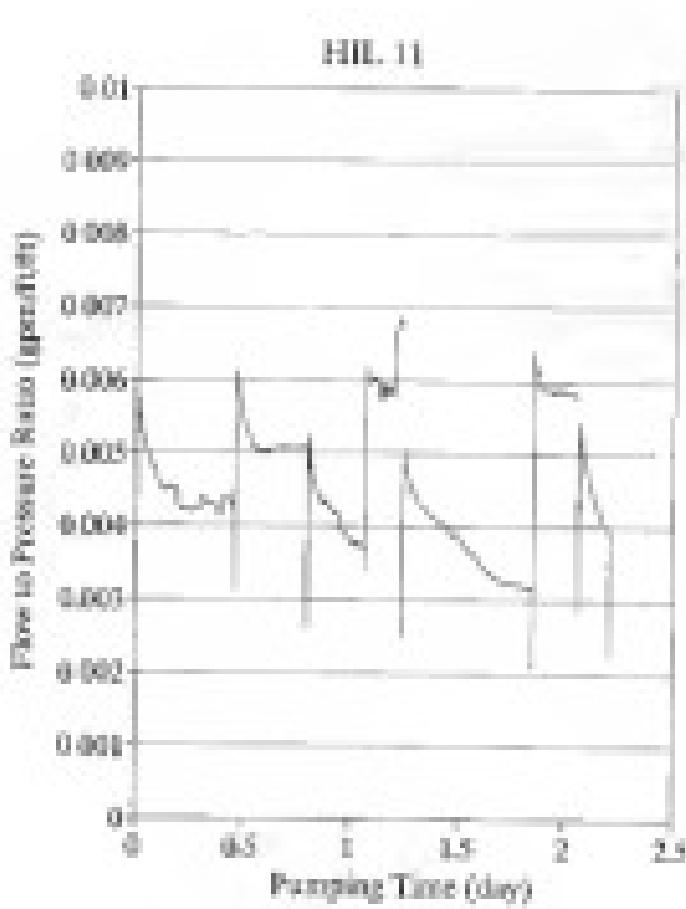


Figure A-48. Δ versus Depression Water HIL. 11

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BIOGRAPHICAL SKETCH

Hector A. Townsend was born in San Diego, California, on October 17, 1947, to Franklin L. and Cynthia Townsend. He graduated from Orange Park High School in Orange Park, Florida, in 1966.

He enrolled at the University of Florida in September, 1969, and graduated with high honors with a Bachelor of Science degree from the Department of Environmental Engineering Sciences in December 1970. He applied to graduate school in the same department in January, 1970, to study solid and hazardous wastes. He graduated with his Master of Engineering degree in December, 1972.

The two married in Orlando, Florida on May 14, 1973.

I certify that I have read this study and that in my opinion it conforms to acceptable standards of scholarly presentation and is fully adequate, in scope and quality, as a dissertation for the degree of Doctor of Philosophy.

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